
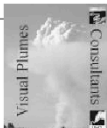


Introduction to Visual Plumes




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Visual Plumes Consultants,
1541 NW Spring Street, Newport, OR 97365, USA



Contents and Schedule

- 1) Purpose and intended audience (Ben Cope and others)
- 2) Visual Plumes (VP) software and systems notes and caveats
- 3) Theoretical basis, emphasis: the Lagrangian UM3 model
- 4) Visual Plumes—familiarization by basic example, the single port plume
- 5) Break
- 6) Multi-port diffuser example
- 7) Special capabilities
 - a) transition to far-field dispersion
 - b) the shallow water approximation technique
 - c) preparing and linking time-series files
 - d) background buildup
- 8) Ramifications
- 9) Questions

Notes (in the “Click to add notes” ppt space) give more detail

 = animation

To help re-establish context for anyone involved subsequent future study of this presentation:

Purpose and intended audience

The purpose of these workshops is to help EPA’s ORD, Regions, and headquarters, as well as tribes, states, and other federal agencies build capacity in mixing zone modeling. The workshops will “demystify” mixing zone studies and provide participants context to understand them. The overarching goals of the workshops are to help participants develop and maintain basic capacity in mixing zone assessment and modeling, train staff on what to look for when reviewing a mixing zone study, discuss current trends in mixing zone assessment and modeling, and encourage collaboration and consistency between EPA regions and state partners with regards to mixing zone assessment and modeling. Specifically, the workshop will train participants on:

1. The basic science behind the mixing of effluent in the environment.
2. What to look for when reviewing mixing zone studies.
3. How various assumptions affect dilution results.
4. How to interpret mixing zone modeling results.

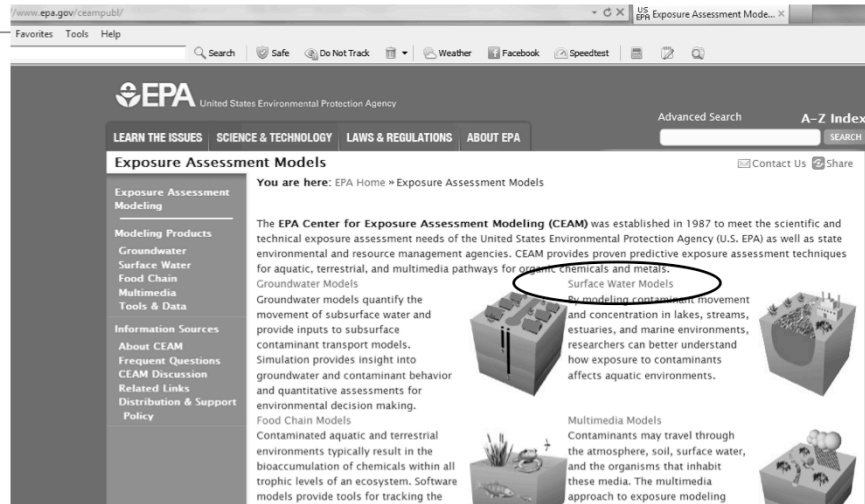
Software and systems notes and caveats

Visual Plumes, a model platform available through EPA:

CEAM at Athens, Georgia: <http://www.epa.gov/ceampubl/>

Manual: <http://www.epa.gov/ceampubl/swater/vplume/VP-Manual.pdf>

Software and update: <http://www.epa.gov/ceampubl/swater/vplume/index.html>



Software and systems: CEAM website

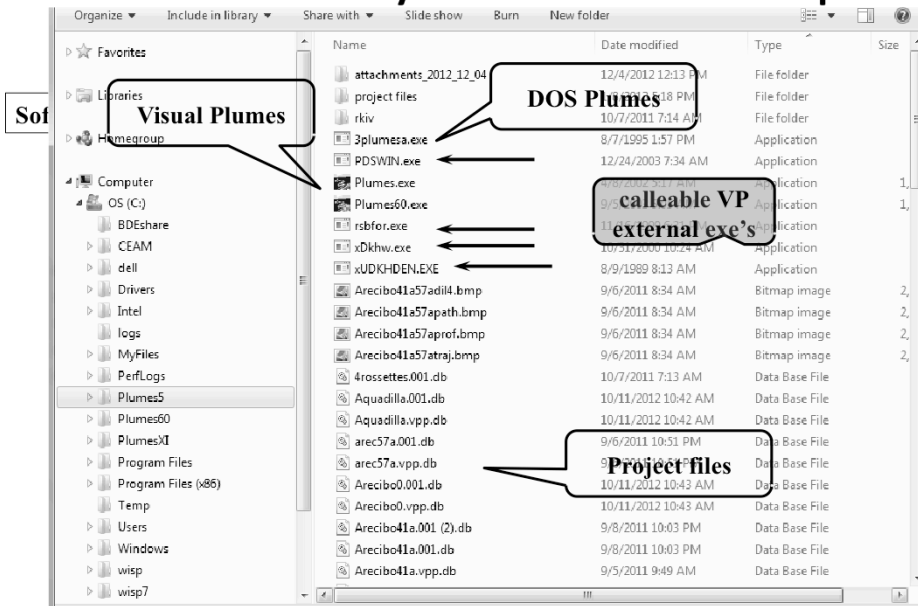
Software and update: <http://www.epa.gov/ceampubl/swater/vplume/index.html>

RUSLE2	Win 98, NT, 2000, XP	rill, interrill, erosion, sediment, overland flow, climate, soil, topography, land use	USDA Agricultural Research Service
SERAFM	MS-Excel 2003	serafm, exposure, assessment, mercury, hg, surface water, pond, stream, river	CEAM
SWMM	Win 98, NT, ME, 2000, XP	aquatic biology, assessment, combined sewer, community, discharge, environmental effects, metals, NPS related, NPDES, streams, surface water, test/analysis, TMDL related	Water Supply & Water Resources Division (NRMRL)
Virtual Beach	MS Windows	surface water, water bodies, beach, pathogen predictor, multiple linear regression, MLR, best-fit model	CEAM
Visual Plumes	Win 98, NT, 2000, XP	surface, water, jet, plume, model, quality, contaminant, TMDL	CEAM
WASP	Win 95, 98, ME, 2000, XP	aquatic biology, assessment, compliance, discharge, environmental effects, hydrology, metals, NPS related, NPDES, point source(s), surface water, test/analysis, TMDL related	Watershed & Water Quality Modeling Tech Support Center (ERD/EPA Region 4)
WHATIF	Win XP(SP2)	watershed, health, fish, habitat, macro-invertebrate, biodiversity, BASS, biomass, biota, aquatic ecosystem, MAHA, CVI, hydraulic, bankfull, flow, restoration, foodweb, mercury, PCB, dioxin	CEAM

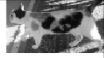
Virtual Beach
Authors of Ver. 1 (Research)
Frick and Ge

CEAM: Home | Products | Information | Archived Models

Software and systems: install and setup



EPA Modeling Webinar 22-24 Jan 2013



After setup:

Software and systems: OS and use issues

Most of VP: Windows XP and earlier
Coding: Delphi 7 (no relation to Windows 7) and earlier
90% interface
Dependence on DLLs
Borland Database Engine (e.g. BDEinfosetup.exe)

Vista, Windows 7, Windows 8
Users Operating System experience
User as novice: most issues can be resolved, not always easily

VP Upgrade example: install the BDE somehow;
then, open Plumes.exe as Administrator; if vptempstorage
error, retry; choose No, start a new project; UM3; if the error
recurs, try again

Notes

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Visual Plumes was developed in Windows XP and earlier versions of Microsoft Windows Operating System (OS). Beginning with Windows Vista it became difficult to compile VP (convert the computer code into executable language) VP. At this time VP is compiled on a Windows 7 machine through a Windows XP emulator. The computer language is Delphi 7 (a superset of Pascal) .

VP uses the Borland Database Engine (BDE), software that supports the handling of the diffuser and ambient tables used in VP. Various other software applications also use the BDE engine. If the BDE engine is installed on any given computer (due to other prior application installations) then VP works directly after installing VP. If not, it is necessary to find a application which will install the BDE components. One such application is called BDEinfosetup.exe. While VPC owns the file, it is not clear that VPC can legally distribute it. Therefore, VPC depends on the user to acquire the necessary software. It may be possible that EPA could bundled the application with VP on the CEAM website.

Users should also be aware that there are a few known bugs in VP that have not been fully identified and corrected. In some instances these are initialization problems that can be overcome by repeating the action again. In any case, the user is invited to report bugs so that future versions of VP may be corrected.

VPC seeks to maintain VP in the public domain and offers to update older versions of VP for inclusion as updates on the EPA CEAM website.

Terms and Definitions

Terms and definitions

Aspiration entrainment: tends to be the dominant entrainment mechanism in low currents, including stagnant ambient; in UM3 it is proportional to the area the plume shares with the ambient fluid; where plumes are merged and are demarcated by vertical reflection planes it is assumed that the plume and its neighbor gain and lose equivalent amounts of mass so that no net entrainment occurs across those vertical surfaces, only over the surfaces still exposed to ambient fluid admittedly

Background buildup technique: an alternative approach to simulating the effects of merging; plumes are not restricted to the reflection technique but rather act in isolation with the effects of merging accounted for through changes to the plume's background conditions, particularly the background pollutant concentration; the approach more closely mimics actual mixing mechanisms but, to be rigorous, would involve not only adjusting the background concentration due to the presence of upstream plumes but the physical environment the plume in question occupies, including all variables and velocities

Co-flowing plumes: the condition where the effluent discharge and the ambient current flow in the same direction

Control volume: the modeling analogue of the plume element in the Eulerian plume model formulation, integral flux equations; unlike the plume element, the model accounts for flux changes as a function of s , the distance along the plume trajectory, the integration step being ds ; the stiffness of the model equations requires management of ds that can lead to discontinuous changes in the endpoint dilution as input conditions are changed only incrementally; also sometimes referred to as the plume element, the analogous Lagrangian control volume

Counter-flowing plumes: the condition where the effluent discharge flows in the opposite direction of the ambient current

Critical Initial Dilution: the flow weighted average of a diffuser plumes' endpoint dilutions; this review recommends that for the purposes of calculating the CID that merged plumes be treated as grouped entities each with their combined CID

Cross-current: ambient current not either co-flowing or counter-flowing will possess a component of velocity that is perpendicular to the plume at the port; cross-currents add another term to the entrainment equations, for example, as in UM3, and will tend to increase overall entrainment in the absence of merging; it is important in reducing the spacing between plumes to values less than the physical spacing

Deep-water assumption: integral plume models such as UD and UM3 were developed with the assumption that water depth would not constrain the motion of the plume; the reason for adopting the assumption was to simplify the theory; the models do not plume-water surface interaction; other steps or models must be taken to model the plume beyond the point where any part of it hits the surface (although some relaxation for slightly grazing the surface might be tolerable)

Densimetric Froude number: this is a similarity parameter that expresses the relative importance (ratio) of kinetic and potential energy inherent in the plume element at the source; small values represent pure plumes that possess little or no initial velocity (like a heated plate), large values are momentum dominated jets with little or no buoyancy perhaps requiring pump pressure to attain the high velocities; in vertical plumes (like natural draft cooling towers) values less than unity are plumes that possess excess buoyancy to briefly accelerate the plume element at the source causing it to stretch out and dynamically contract its diameter, the analogous mechanism experienced in seawater intrusion; finally, the similarity property allows plumes to be compared across spatial scales, plumes with the same similarity parameters exhibiting the same morphology (plume shape) when plotted in dimensionless terms (for example, in terms of diameters downstream and vertically)

Notes

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UDKHEN: a version of UDKHDEN that was developed explicitly for use with Visual Plumes (Frick et al. 2004); replaced in this review by an updated version of

This slide is intended as a reference for future study

Dilution Models for Effluent Discharges

4th Edition
(Visual Plumes)

Recommended Tutorial



by

W.E. Frick¹, P.J.W. Roberts², L.R. Davis³,
J. Keyes⁴, D.J. Baumgartner⁵, K.P. George⁶

¹ Ecosystems Research Div., NERL, USEPA, Athens, Georgia 30605-2700

² Georgia Institute of Technology, Atlanta, Georgia 30332

³ CH2M HILL, Corvallis, Oregon 97330

⁴ Brown and Caldwell, Atlanta, Georgia 30346

⁵ University of Arizona, Tucson, Arizona 98706

⁶ Alaska Department of Environmental Conservation, Juneau, Alaska 99801

4 March 2003

Ecosystems Research Division, NERL, ORD
U.S. Environmental Protection Agency

960 College Station Road
Athens, Georgia 30605-2700
EPA Modeling Web page 22-24 Jan 2013

Get the VP
manual!!
Tutorial starts
on page
4.7 to 4.20

Visual Plumes, Ver. 1.0; U.S. Environmental Protection Agency, ERD-Athens, ORD, 22 July 2001
File Edit Models Stop Run Help

Visual Plumes Manager/ Model Platform

Diffuser: Fan-Run-16.vpp.db | Ambient: C:\Plumes\Fan-Run-16.001.db | Special Settings | Text Output | Graphical Output

Project: C:\Plumes\Fan-Run-16

Ref: Fan, L.N.1967. Turbulent buoyant jets into stratified or flowing ambient fluids. KH-R-15, Keck Lab, Cal Tech, CA.)

Input data on p. 61, elevation view on p. 69 (digitized in file Fan16.txt, use Verify button to bring into Visual Plumes).

Notes: Plume plotted from Fan's O' origin with depth arbitrarily assigned at approximately 1m. Initial and ambient temps. and salinities (and densities) are slightly off due to source not set exactly at 1.00m. The density column is set to

Ambient file list


Filename	Cases
C:\Plumes\Fan-Run16.001.db	11

After run go to tab:

- ☐ Diffuser
- ☐ Ambient
- ☐ Special
- ☐ Text
- ☒ Graphics

Units Conversion:

- ☒ Convert data
- ☐ Label only



Model Configuration

- ☐ Brooks far-field solution
- ☐ Graph effective dilution
- ☐ Average plume boundary
- ☐ Amb. current vector averaging
- ☐ Tidal pollution buildup
- ☐ Same-levels time-series input

Case selection:

- ☒ Base or selected case
- ☐ Sequential, all ambient list
- ☐ Sequential, parse ambient
- ☐ All combinations

VP's main tab:
the Diffuser tab

Diffuser, Flow, Mixing Zone Inputs

Port diameter	n/t	Port depth	Port flow	Port density	Port temp	Port conc	Acute mix zone	Chronic mix zone	Port depth	Effluent flow	Effluent density	Effluent temp	Effluent conc	
m	m	m	deg	deg	m	g	g	g	m	MLD	sigmaT	C	ppm	
0.0025		0.1	0	0	1	5			1	2	1.012	0.00267	0.001	20

Parameters for selected row

Frroude number	25.28
Eff density (kg/m3)	1000.001
Port vel (m/s)	0.63
P-da (m)	0.0025
P-da (m)	2.5000E-3
Case No.	1.0

Time Series-Files (optional)

Time-series filename	Port depth	Effluent flow	Effluent density	Effluent temp	Effluent conc
click for file	click for file	click for file	click for file	click for file	click for file
Time increment (hrs)					
Time cycling period					
Measurement unit					

Borrow time-series from project: C:\Plumes\Fan-Run-16

Port depth	Effluent flow	Effluent density	Effluent temp	Effluent conc
click for file	click for file	click for file	click for file	click for file
Time increment (hrs)				
Time cycling period				
Measurement unit				

Visual Plumes, Ver. 1.0; U.S. Environmental Protection Agency, ERD-Athens, ORD, 22 July 2001

File Edit Models Stop Run Help

Diffuser: Fan-Run-16.vpp.db Ambient: C:\Plumes\Fan-Run-16.001.db Special Settings Text Output Graphical Output

The Ambient tab

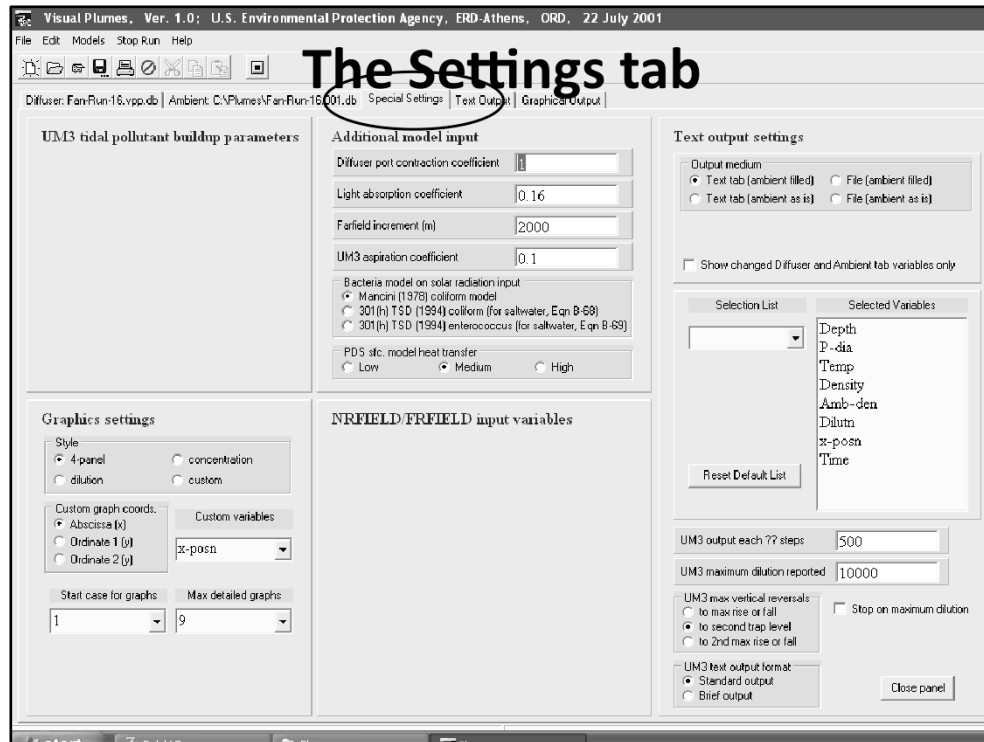
Ambient Inputs

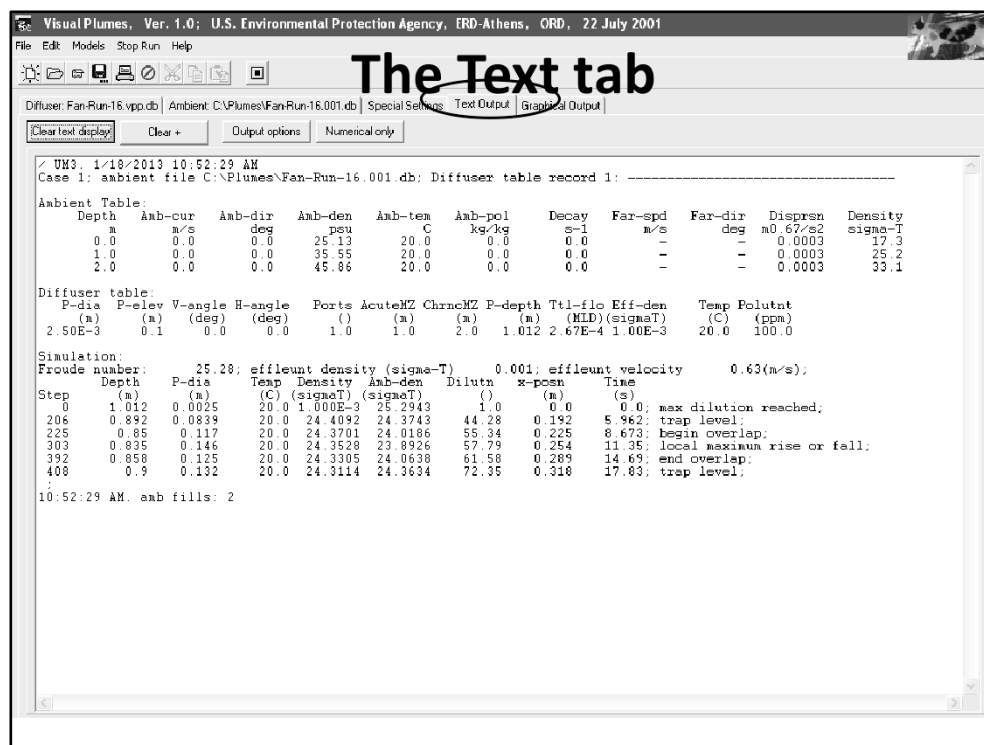
	Measurement depth or height	Current speed	Current direction	Ambient salinity	Ambient temperature	Background concentration	Pollutant decay rate(1)	n/1	n/1	Far-field diffusion coeff
Depth or Height	depth	depth	depth	depth	depth	depth	depth	depth	depth	depth
Extrapolation (sf)	constant	constant	constant	constant	constant	constant	constant	constant	constant	constant
Extrapolation (bfn)	constant	constant	constant	extrapolated	constant	constant	constant	constant	constant	constant
Measurement unit	m	m/s	deg	sigmaT	C	ppm	s-1	m/s	deg	m ² /s ²
	0	0	0	17.3	20	0	0			0.0003
	1			25.2	20					
	2									

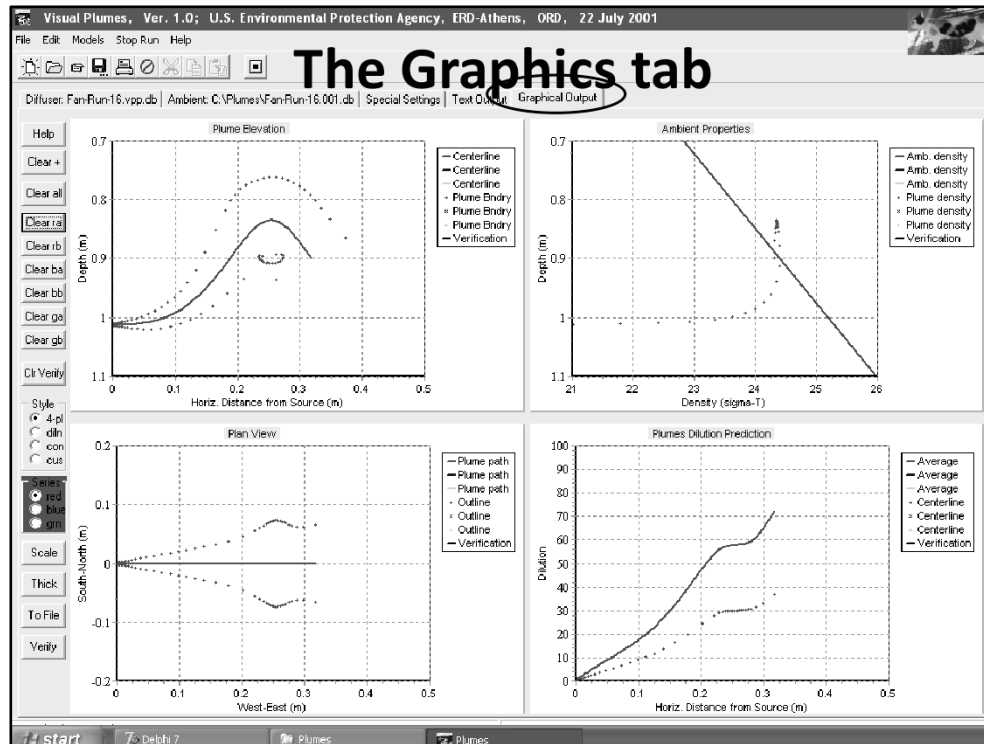
Ambient file list
Filename
Fan-Run-16.001.db 1 1

Time-Series Files (optional) Borrow time-series files from project: C:\Plumes\Fan-Run-16

Time-series filename	click for file	click for file	click for file	click for file	click for file	click for file	click for file	click for file	click for file	click for file
Time increment (hrs)										
Cycling period										
File measurement unit										







Diffuser Peculiarity.vpp.db
Ambient: C:\PlumesX\Necularity.001.db
Special Settings
Text Output
Graphical Output

Project C:\PlumesX\Necularity

Project "C:\PlumesX\Necularity" memo
The basis of this project was that a user identified an instance of the degenerative effluent-ambient velocity matching problem. When the velocities are identical and co-flowing there is no forced entrainment or aspiration and the predictions are anomalous

Files
C:\PlumesX\Necularity.001.db 1 1
C:\PlumesX\Necularity.002.db 1 1
C:\PlumesX\Necularity.001.db 1 1

Enter run go to tab
☒ Diffuser
☐ Ambient
☐ Special
☐ Text
☐ Graphics

Units Conversion
☒ Convert data
☐ Label only

Model
☐ Brooks fa
☐ Report el
☐ Current v
☐ Tidal poll
Case select
☒ Base or
☐ Sequen
☐ Sequen
☐ All comb

Diffuser, Flow, Mixing Zone Inputs

Port diameter	Vertical angle	Horizontal angle	Source x-coord	Source y-coord	Num of ports	Port spacing	n/t	n/t	n/t	Mix zone distance	Isopleth value	Port depth	Effluent flow	Effluent salinity	Effluent temp
m	deg	deg	m	m		m	s	s	s	m	concent	m	m ³ /s	psu	F
0.057	0	0	0	0	1	999				1	0	3.7	0.00053	0	70
0.058	1														
	1														

Insert line (insert)
Delete line (^delete)
delete preceding lines
delete this and following lines
Paste from clipboard (^V)
Font pitch
Help
Cancel

Parameters for selected row

Froude number	
Eff density (kg/m ³)	
Port vel (m/s)	
Spacing (m)	999.0
Spacing (m)	999.0
Case No.	1

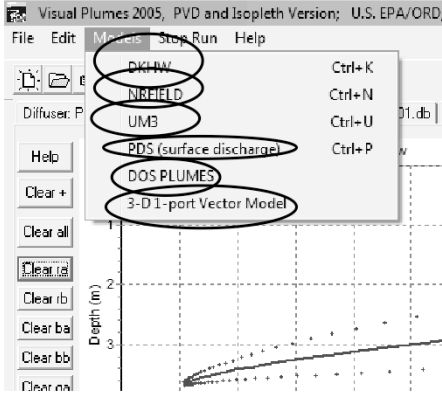
Time Series-File

Time-series filename	click for file	click for file	click for file	click for file	click for file
Time increment (hrs)					
Time series period					
Time series period					
Measurement unit					

Time series from project: C:\PlumesX\Necularity

Effluent salinity	Effluent temp	Effluent conc

Visual Plumes Model Suite



DKHW: Physics-based exe, Eulerian numerical formulation, integral flux model. One or multi-port diffusers.
NRFIELD: Empirical, dimensional analysis and curves fit to data; exe. Based on T-risers, for 4 or more ports.
UM3: Physics-based native, Lagrangian numerical formulation, material element model. One or multi-port diffusers. el
PDS: Eulerian integral flux surface plume model; exe. Buoyant discharges

DOS Plumes: predecessor of Visual Plumes, runs RSB (pre-NRFIELD) and UM (Updated Merge model; pre-UM3). Features auto cell-fill: displays similarity parameters, length scales, cormix classes.

Dreamware prototype depicts wire-mesh graphics, like UM3, vector based.

All but PDS link to the Brooks far-field algorithm, far-field dispersion model.

Notes

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Models such as DKHW are external executable files (exe). VP sets up their input files, calls the exe, waits for the exe to finish, then looks for the output file, reads it, and interprets the information on the text and graphics tabs. Problems can arise when the exe terminates abnormally. A file handling problem can arise when VP then reads an older output file, which is not always apparent when several consecutive cases are involved.

UM3 is a native model so called because it is coded into the VP code. This makes for easier control for the developer as model and interface are compiled together.

DKHW, NRFIELD, and UM3 are initial dilution models that can be linked with the Brooks far-field model.

What is in the names:

DKHW: Physics-based exe, Eulerian numerical formulation, integral flux model. One or multi-port diffusers.

Acronyms: Davis, Kannberg, Hirst model (w = Windows; Windows VP package). Previous versions DKHDEN, UDKHDEN (1985).... Later compilations up to 2011....

NRFIELD: Empirical, dimensional analysis and curves fit to data; exe.

Based on T-risers, for 4 or more ports. RSB in DOS Plumes, native, Roberts, Snyder, Baumgartner model. Roberts continues work on NRFIELD currently conducting experiments with dense discharges.

UM3: Physics-based native, Lagrangian numerical formulation, material element model. One or multi-port diffusers. Merge (pre 1985), UMERGE (1985), UM (1993), UM3, Updated Merge 3-D model.

PDS: Eulerian integral flux surface plume model; exe. Buoyant discharges. Acronym: Prych, Davis, Shirazi model.

DOS Plumes: predecessor of Visual Plumes, runs RSB (pre-NRFIELD) and UM (Updated Merge model; pre-UM3). Features auto cell-fill: displays similarity parameters, length scales, cormix classes.

Dreamware prototype depicts wire-mesh graphics, like UM3, vector based.

Brooks far-field algorithm is a set of equations for estimating dispersion (dilution) in the far-field, beyond the initial dilution phase of plume development.

More to come



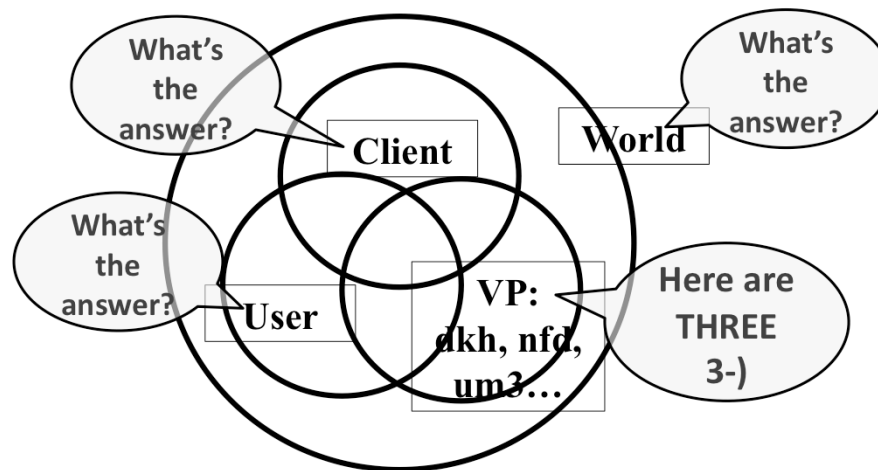
There is more to follow on empirical, hydrodynamic fluid dynamic codes, empirical, Eulerian integral flux and Lagrangian plume models.

**explain
illustrate
“demystify”
touch on basic principles of physics
mathematical formulations
modeling assumptions
UM3 examples (built into Visual Plumes--not an external application)
examples chosen for simplicity, generality, and teaching potential**

VP is public domain software

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Mixing Zone analysis

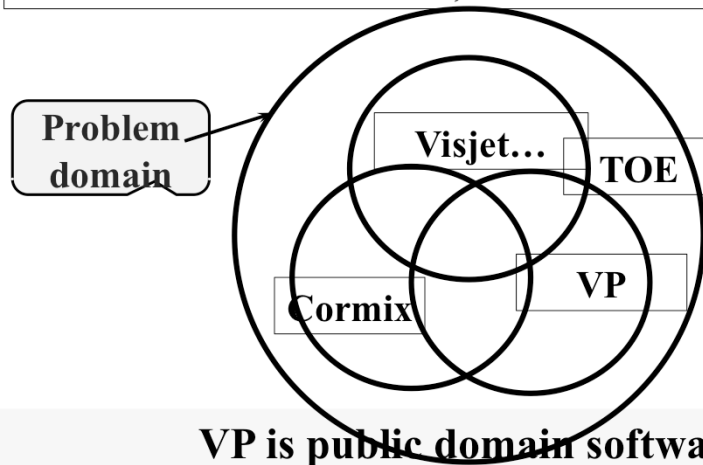


Answers, yes, but no one knows it all (otherwise there'd one). MZ analysis is a partnership

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The problem/model universe

Whom to believe, *best*? How feasible?



VP is public domain software

Everyone can be on the same page

Facilitates inter-model comparison & competition

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Mixing effluent in environment—basic science

Before illustrating by example:

**Let us take a brief tour of plume
problem, physics, and prediction**

Touch on:

capabilities

limitations

pitfalls

mystery and ambiguity

And end with promise:

A bonus rule

Reason for optimism and confidence

Notes

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Even at its simplest, plume modeling guidance can appear mysterious and ambiguous. Understanding the capabilities and limitations of available models can help avoid pitfalls and confusion and promote confidence in model outputs. This section seeks to help the user demystify the art and science of plume modeling for themselves.

Conceptual model in a snapshot: it's air but, by similarity, it could be water

Some questions:
Current?
Steady?
Cross-section round?
Jet or plume?
Phase changes?
Ambient stratification?
Dimension imply dilution?

plume

source

Receptor
(somewhere)

other plumes

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Why not the TOE for Visual Plumes?



Theory of Everything

“A theory of everything (ToE) or final theory is a putative theory of theoretical physics that fully explains and links together all known physical phenomena, and predicts the outcome of any experiment that could be carried out in principle.”

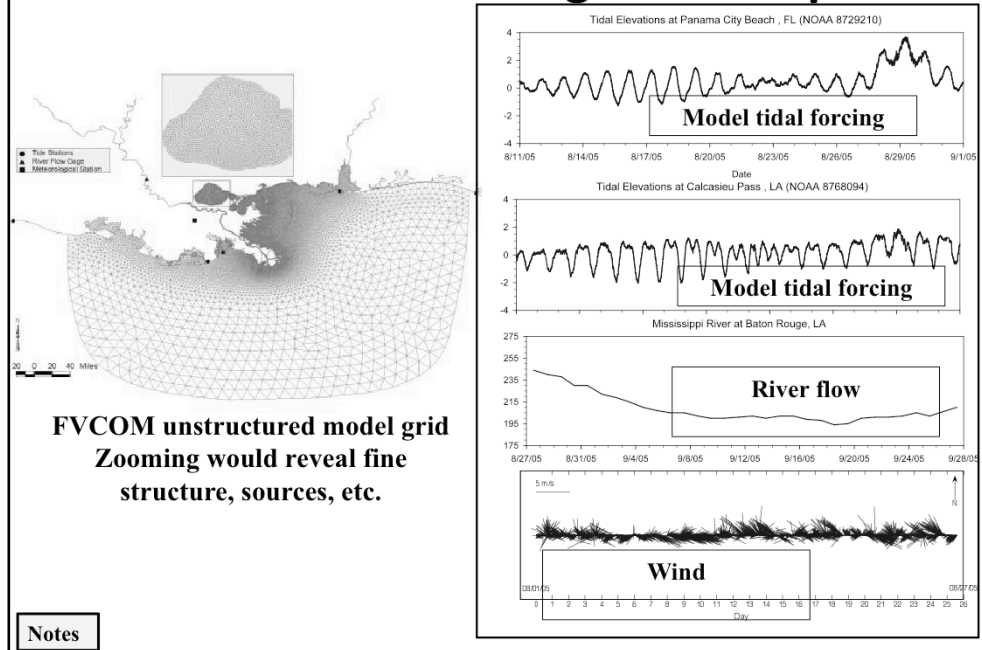
http://en.wikipedia.org/wiki/Theory_of_everything

In plume modeling this dream is called Computational Fluid Dynamics (CFD). In principle a comprehensive CFD model could model any plume in relationship to other plumes and their bathymetric, chemical, and physical environments. All that is required is precise and accurate knowledge of

**Initial conditions (IC)
Boundary conditions (BC)
Forcing functions
Chemistry
Physics
Thermodynamics....**

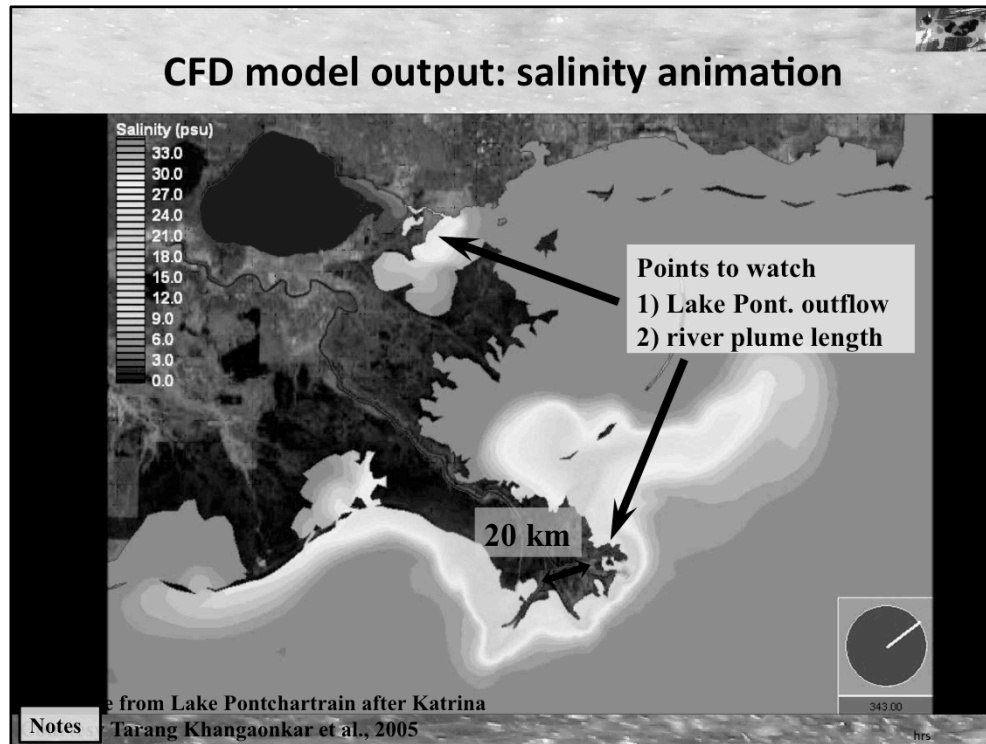
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Meet a CFD model: grid and input

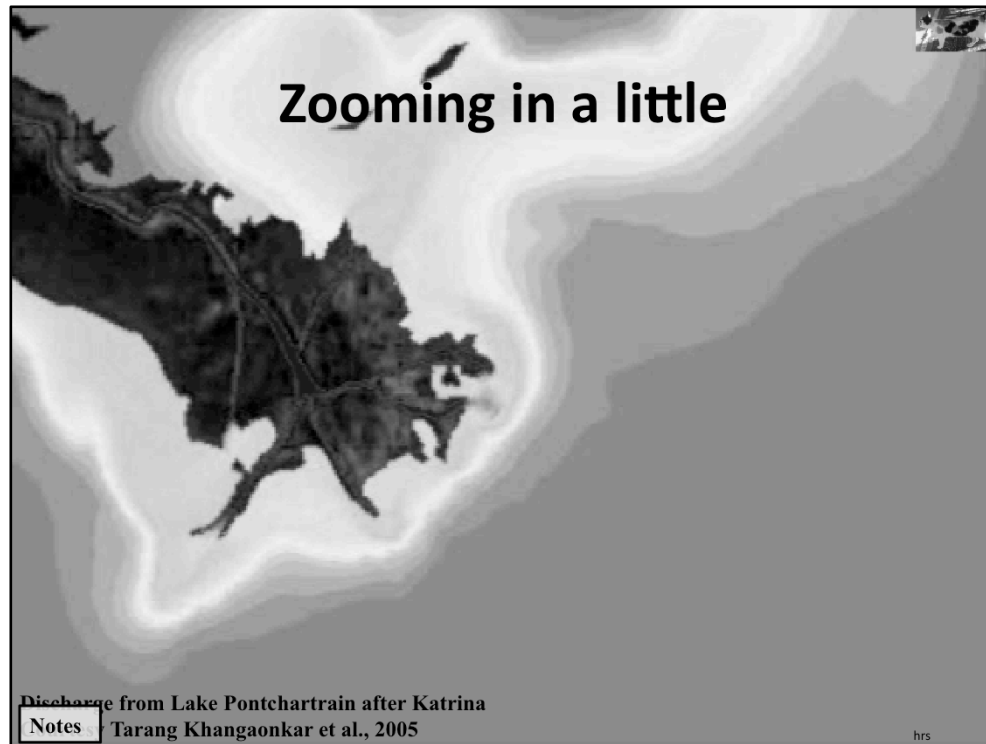


This work concerned events surrounding Hurricane Katrina, 2005.

Note the Mississippi River flow at Baton Rouge, 6000 cubic meters per second equals about 212,000cfs. This is about 3 times larger than the tidal Yaquina River, Oregon, however, the Mississippi has multiple mouths, including the Atchafalaya River that discharges near Morgan City, west of New Orleans (not shown here). (This note refers to another comparisons including use of the Visual Plumes PDS river discharge model.)



Another output of the modeling. Note the intense parts of the plumes penetrate about 5km into the Gulf.



The intense parts of the plumes penetrate about 5km into the Gulf.

Done! Except....



In theory, we can accurately model plumes using accurate CFD models.

However, consider the

Resources

Setup

Data collection (IC, BC....)

Expense....

We (modelers, users...) must formulate dispersion coefficients everywhere (eddies and turbulence) (models in themselves)

A dream for most of us. On to Visual Plumes' imperfect answers.

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One alternative: empirical modeling

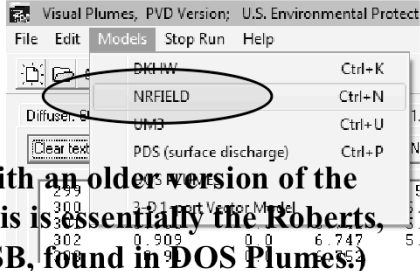
While we wait for CFD, how about going to the laboratory for solutions? Empirical models.

Visual Plumes comes bundled with an older version of the NRFIELD empirical model. (This is essentially the Roberts, Snyder, Baumgartner model, RSB, found in DOS Plumes.) NRFIELD is a stand-alone executable that can be called by VP:

- VP creates the input file
- VP initiates NRFIELD execution
- VP reads the output file and displays output

Considerations:

- NRFIELD addresses multiple merging plume problems
- It is an endpoint model.

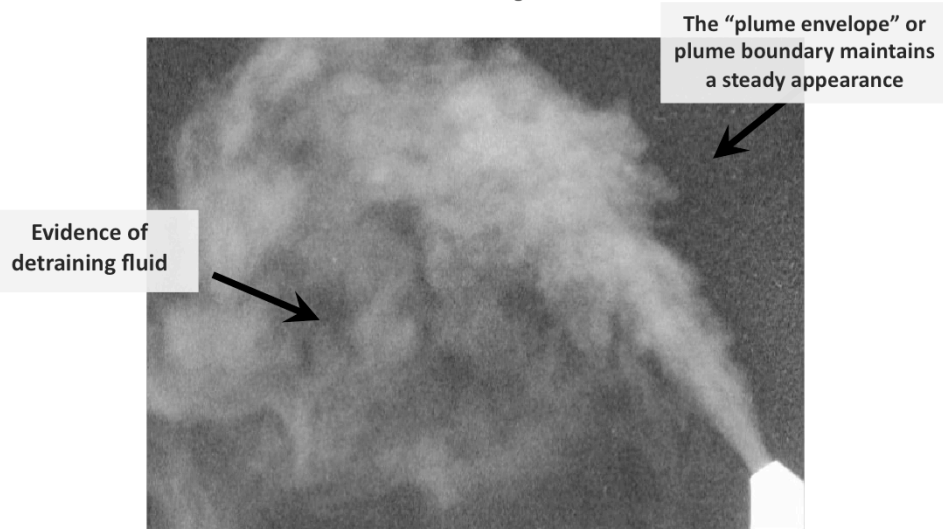


Notes

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Empirical models are based on laboratory measurements. Lab results may be fitted to model parameters that are derived through dimensional analysis or other techniques. Coefficients are established that produce the best fits and similarity theory may be used to generalize the results, making it possible to adapt results to larger or smaller length scales. Similarity may be achieved by matching Froude number, stratification number, Reynolds number and other similarity parameters or length scales. Non-linear effects like the density of water near freezing temperature can complicate similarity theory, sometimes with unexpected and significant consequences.

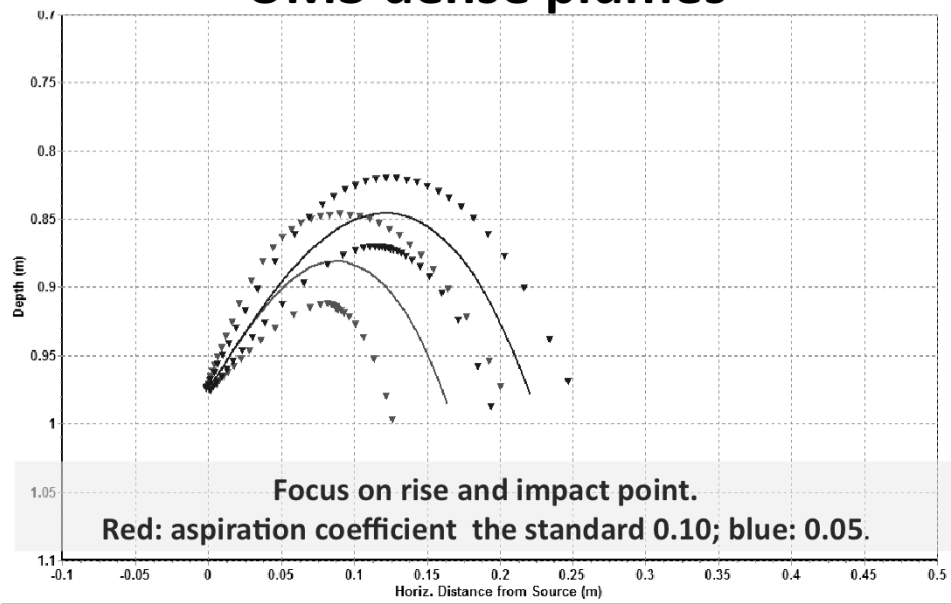
A dense plume



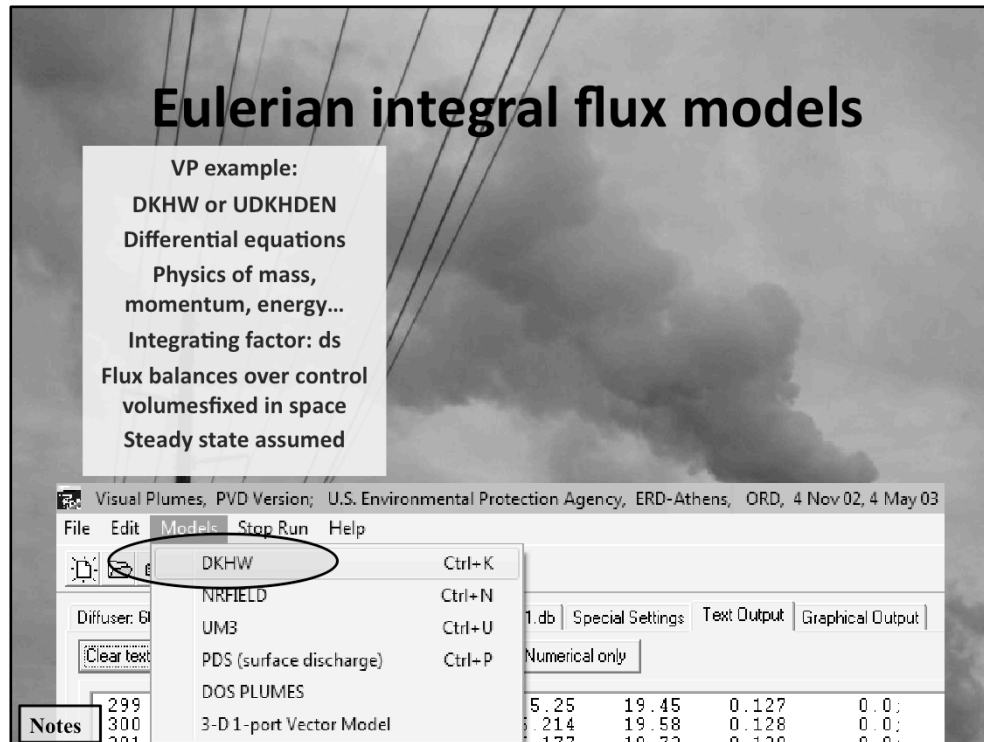
A household dehumidifier plume showing evidence of unexpected behavior. Mimicking the laboratory, will NRFIELD be the first model modified to explain observations?

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UM3 dense plumes



EPA Modeling Webinar 22-24 Jan 2013



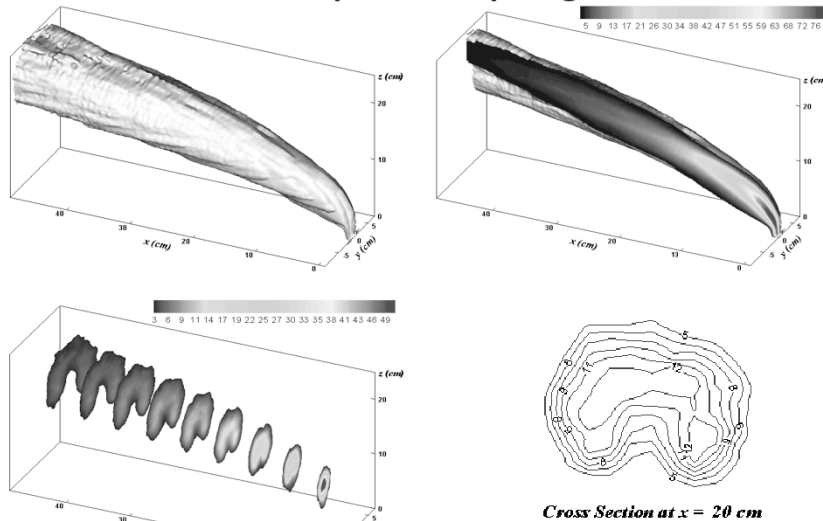
Corjet, one of the models in Cormix, is also an Eulerian integral flux model.

DKH refers to Davis, Kannberg, and Hirst, the original authors of DKHden even before the UDKHDEN and UMERGE (now UM3) models were published in the EPA publication of EPA/600/3-85/073a and b: "Initial mixing characteristics of municipal ocean discharges" in 1985. (Muellenhoff, Soldate, Baumgartner, Schuldt, Davis, and Frick.) The U stood for Universal because each included model used the same input format called Universal Data Files (UDF) files. UM3 now might suggest the "Updated Merge 3-dimensional" model. UMERGE was a quasi 3-D model whereas UM3 is fully three-dimensional when modeling individual plumes, making full use of vector algebra to represent three-dimensional physics.

Cautionary DKHw and UDKHDEN notes for the record:

- 1) they do not report when the plumes intersect the receiving water surface
- 2) they hold plume spacing constant even when the current is not perpendicular to the diffuser axis (to be conservative the user should input the reduced spacing, the spacing distance projected to the current)

Unstratified buoyant jet in the lab Conceptual morphing



**We see evidence of steady state, time-averaging,
plume morphology (round plume assumption)...**

Notes

This presentation covers a lot of ground. For the sake of time some aspects of modeling are emphasized at the expense of other aspects. The previous Eulerian model simulations are based on the concept of steady state. This means that the predictions represent time-averaged behavior. We may think of averaging together many snapshots of the instantaneous plumes that are quite turbulent and heterogeneous. The result of this averaging is to produce smooth surfaces and concentration patterns as shown in the upper right panel. It is such patterns and concentrations we attempt to simulate. To make the problem tractable we assume the cross-section is round but already recognize that this is a simplification which can have significant consequences. In current the plumes are often kidney shaped as shown in the lower right panel. If stratification is strong the cross-section can become even more flattened in shape. This can affect our interpretation of when the plume's upper surface intersects the water surface.

How does numerical Eulerian method work?



Define the source:

IC, BC..
velocity vector ↑
radius
temperature ●
salinity ○
concentration ●
current ←
orientation...

Conservation of mass (4.1)

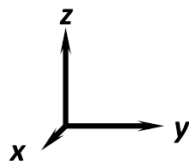
$$\frac{d}{ds} \int_0^\infty \bar{u} r dr = E$$

$$\left(\int_0^\infty \bar{u} r dr \right)_{s+\Delta s} = \left(\int_0^\infty \bar{u} r dr \right)_s + E \Delta s$$

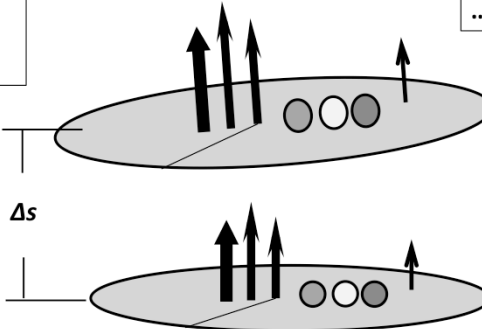
Derive (compute)...

density
buoyancy
area...
mass flux ↑
momentum flux ↑
energy flux ↑
...

Define coordinate system and location

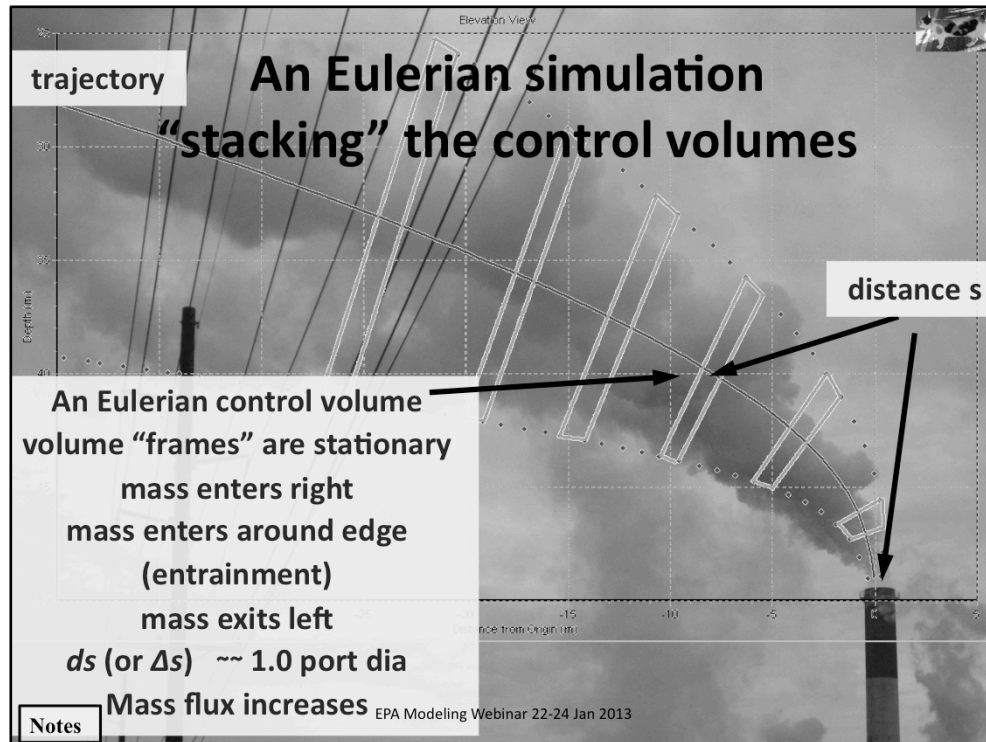


Δs



By the way, the integral $\int_0^\infty \bar{u} r dr$ is the mass flux





This simulation is not based on actual input conditions, which are unknown. This is a crude example of similarity. The actual medium is air, the model medium is water. Input conditions were varied until a fit, relative to a common diameter, was obtained. Output was set up to plot diameters (denoted by red dots) and at constant intervals to help represent the concept of control volumes.

Shown is a UM3 simulation. UM3 was modified to output plume diameters (diameter endpoints) whenever the travel distance increased by more than the criterion distance after the previous diameter output. The apparent lengths ds of the control volumes, which should be equal, differ slightly from one control volume to the next because the integration step is variable and finite (though small). As several steps of variable size are involved between outputs, the accumulated distance varies from one cross-section to the next.

The control volume length could be varied as part of a model convergence scheme but the main idea is that the volumes are stationary with mass flux in (from the source, from the upstream control volume, or from the surroundings) or out (to enter the downstream control volume).

Any handy laws/rules on dilution?



As the fluid entering the bottom of the control volume, augmented by the entrained fluid coming in from the ambient, all exits the top of the control volume we may ask:

At some travel distance s , is dilution approximately directly proportional to the area of the cross-section of the plume?

Yes or no?

Other than holding the plume shape constant, the significance of steady state is a little obscure (implicit?) with Eulerian models. Does it help answer the question? More to follow.

Notes

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Finite difference plume model comparison

We just saw the Eulerian integral flux formulation

The infinitesimal distance ds is the integrating factor

Differential equations express fluid dynamics (physics)

e.g. conservation of mass: $\frac{d}{ds} \int_0^\infty \bar{u} r dr = \text{entrainment}$

where the integral is consistent with the choice of control volume

In finite difference models ds is expressed by $\Delta s = s_2 - s_1$, which is small

Other equations, e.g. eqn. of state, bookkeeping,... round out the model

With the Lagrangian integral flux formulation we will find

The infinitesimal time dt is the integrating factor

The control volume is called the plume element

It is a material (coherent) element

Again, differential equations express fluid dynamics (physics)

e.g. conservation of mass: $\frac{dm}{dt} = \text{entrainment}$

where $m = \rho_{\text{plume element}} \text{vol}_{\text{plume element}}$

In finite difference models dt is expressed by $\Delta t = t_2 - t_1$, which is small

Again, other equations, e.g. eqn. of state, bookkeeping,... round out the model

Notes

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The DOS Plumes manual covers the Lagrangian theory in some detail. The first journal article to outline the complete plume theory (excluding merging and other out of scope complications) was published in 1984. The finite-difference model, which is very useful for understanding the practicalities of numerical modeling of this type, is found in EPA-600/3-76-100 (Cooling tower plume model), 1976.

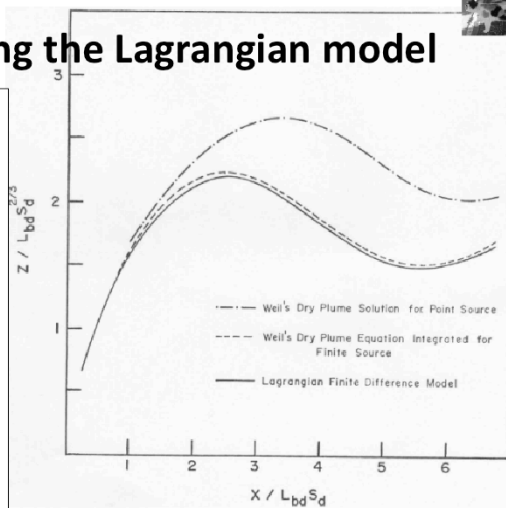
Replication: proving the Lagrangian model

Eulerian plume models came first
(Fan 1967, Weil 1974....)

Late to the party, when Winiarski
& Frick developed the Lagrangian
plume model formulation they set
out to prove its equivalence to the
Eulerian formulation

This was successful given the same
assumptions: a round plume,
steady state, equations of state,....

The proof was published and
clarified the initial conditions of
Weil's Eulerian plume model
integration (upper and middle
traces).



Reprinted from JOURNAL OF APPLIED METEOROLOGY, Vol. 14, No. 5, April 1975, pp. 421
American Meteorological Society
Printed in U. S. A.

Comments on "The Rise of Moist, Buoyant Plumes"

WALTER FRICK AND LARRY WINIARSKI

Thermal Pollution Branch, Environmental Protection Agency, Corvallis, Ore. 97330
27 December 1974

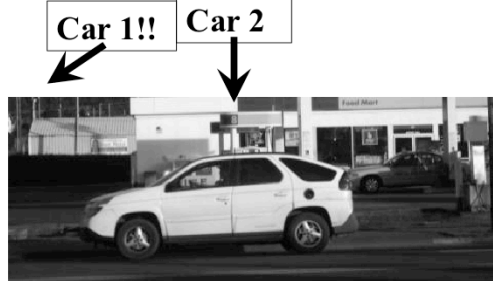
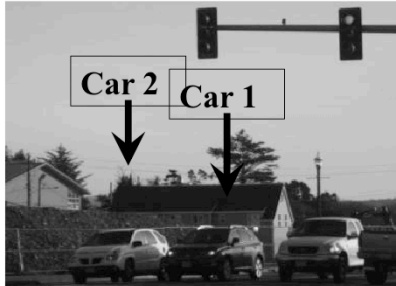
Notes

EPA-Moc

Presumably no Eulerian modeler has to prove equivalence with the Lagrangian formulation ☺

steady state leads to bonus ? answer

Two cars stopped, after they start how far apart are they when they reach the open road traveling, say, 60mph (88fps)?



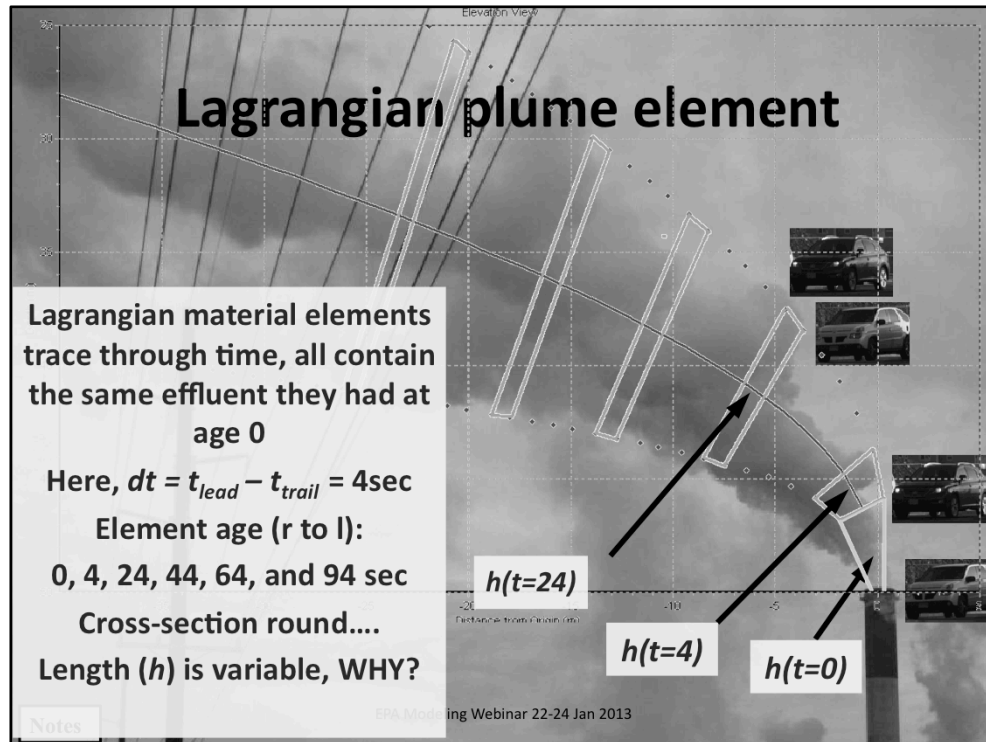
Trick question, we don't know the answer. However, we would if
(1) we knew the time between Car 1 and Car 2 starting, and,
(2) both drivers drove identically (same time history, steady state).

E.g., if they started 1.00sec apart, they would always be 1.00sec apart, which translates to 88ft at 60mph, 44ft at 30mph, etc.

Notes

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Actually, a more useful analogy to plumes would be two cars possessing the same speed as they pass through the light but car 2 passing that point one second behind car 1. If they practice the same driving pattern (steady state) their distance apart will either increase or decrease depending on whether they speed up or slow down down the road. Now you know why trucks are usually closer together on steep grades. They may be spacing themselves, say, 2 seconds apart.



In Lagrangian theory all the material in the plume element at its inception remain in the plume element. In this sense it is a material element. Its increase in volume is due to entrainment plus changes in density that come about from water's density non-linear response to salinity and temperature.

As the leading and trailing faces occupy position a given amount of time different in age, $h = (\text{instantaneous speed})(t_2 - t_1)$. Given steady state, the height h is only a function of the instantaneous speed because $t_2 - t_1$ is constant while steady state is maintained.

Actual plume elements are shorter, exaggerated here for instructional purposes. In initializing conditions UM3 sets $h(0)$ to one-tenth of the initial diameter. The initial time step $(\Delta t)_0$ is correspondingly small.

Steady state and plume element length, h ; the “free” equation gives the answer

Referring to Figure 65, $\Delta|Z|$ is seen to be the difference in velocity at two opposing faces of the semi-infinite element. (The velocity vectors are proportional to the displacement shown. Also, in both formulations, the element is infinitesimal only along its trajectory, thus it is a hybrid infinitesimal volume which is treated differently from truly infinitesimal volume elements.) Since the Lagrangian formulation is used with material elements and it is assumed the velocity is uniform, the faces separate or converge, proportional to $\Delta|Z|$, i.e.,

$$\Delta h = \Delta|Z| \delta t \quad (29)$$

where δt is an arbitrary, but constant, time increment. Integrating Equation 29 and noting that the corresponding speed differentials and lengths are $\Delta|Z|$ and h_o , and $\Delta|Z|$ and h yields

$$\int_{h_o}^h dh = \delta t \int_{u_{so}}^{u_s} du_s$$

where $u_s = |Z|$ and $u_{so} = |Z_o|$. Equation 30 can be integrated to yield

$$h - h_o = (u_s - u_{so})\delta t$$

Finally, since δt can be chosen to be h/u_{so} ,

$$\frac{h}{h_o} = \frac{u_s}{u_{so}}$$

and $|Z|$, i.e. u_s and h change proportionally.

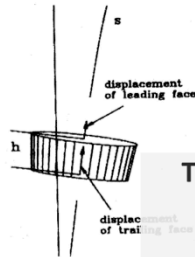


Figure 65. Convergence of element faces due to differences in face velocities.

$$\frac{h}{h_o} = \frac{u_s}{u_{so}}$$

The mass of the plume element

$$m = \rho \pi h r^2$$

or

$$r = \sqrt{\frac{m}{\rho \pi h}} \quad (30)$$

Thus r is not only a function of the mass of the plume element but also its height (or length) h

The answer to the poll question is NO

Notes

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This effect is sometimes referred to as the “jelly sandwich” equation. Squeeze both ends and the diameter increases. Pull both ends outward, like bellows, and the diameter decreases. This is in the absence of entrainment, which may mask some of the jelly-sandwich effect.



Corollaries (bonuses)

A plume discharged to high current will be thin

(Dye studies in high current areas will have trouble finding the plume)

A plume discharged to low current will be fat, surface hit issues

The “free” equation completes the equivalence with the Eulerian formulation

Explicit with UM3, these truths are implicit in the Eulerian models

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UM3 skeleton or flow chart



Define initial conditions (IC): element mass m , properties (temperature T , salinity, time, position...), radius r , and, of course, h (or h_o) and Δt

Define boundary conditions (BC): ambient properties (temperature T , salinity, current, concentration, decay), stratification of properties

Begin model loop
Bookkeeping: interpret and interpolate the ambient array of properties

Calculate Δm , the mass entrained into the plume element in the time step Δt . Requires an entrainment function

Calculate new element properties by mixing m and Δm . E.g., new salinity:

$$S_{t+\Delta t} = \frac{S_t m + S_{amb} \Delta m}{m + \Delta m}$$

Apply equation of state (ρ, S, T); calculate dynamics: momentum, energy, buoyancy; calculate displacement (new position)

Use the “free” eqn. (h) (steady state) to solve for radius: $r = \sqrt{\frac{m}{\rho \pi h}}$

More bookkeeping, like output. Finally, return to the beginning of the model loop

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The name of the game: entrainment



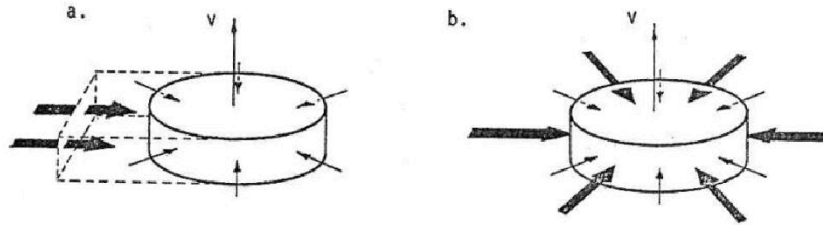
Considering that identical assumptions result in Eulerian integral flux and Lagrangian model equivalence, what sets integral models apart are the assumptions (if the underlying assumptions are different)

- (1) entrainment hypotheses (functions)**
- (2) numerical convergence scheme**
- (3) ancillary capabilities like plume merging and treatment of surfaces**
- (4) Facilities: unit conversion, time-series input, and other capabilities or constraints**

Given the assessment satisfies the underlying assumptions used in model development (viz. deep water and steady state) the entrainment functions deserve the greatest attention.

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Early entrainment conception

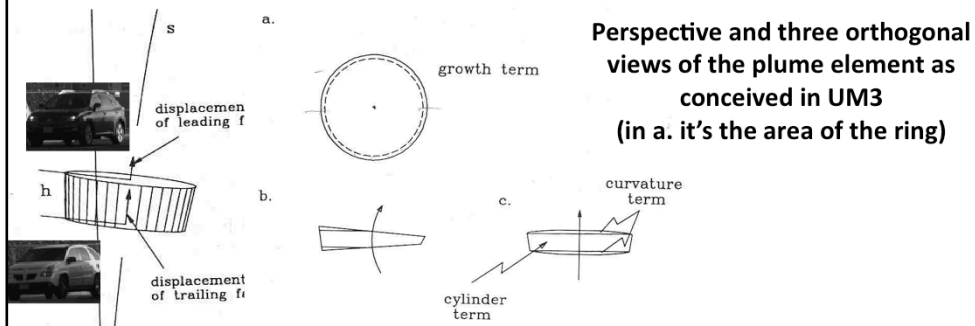


historical context

- a) forced entrainment due to current (more next 3 slides)
- b) aspiration entrainment due to suction: this mechanism is due to the Bernoulli effect; the inflow velocity is proportional to the surface area of the element and the velocity shear between the average plume element velocity and the ambient velocity; it is governed by an adjustable aspiration entrainment coefficient

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Projected Area Entrainment (PAE)



The PAE hypothesis postulates forced entrainment =

$(\text{ambient density}) * (\text{current}) * (\text{total area projected to the current})$

Total projected area of the plume element (3D conception) =

(a) growth + (b) cross-flow + (c) cylinder and curvature

The PAE hypothesis appears to require no adjustment; the coefficient is 1.0.

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Follow science for the answer--yes, but...



Before recognizing the significance of steady state (aka jse)

Developing the Lagrangian “pre-UM3” from scratch took about a year.

**?About how many entrainment assumptions/hypotheses did W&F try in the effort to obtain good fit to Fan’s data?
1, 2, 5, 10, 20, 50?**

**?After adding the “free” equation for plume element length, how many revisions before formulating the forced entrainment equation as a function of r , h , and θ ?
1, 2, 5, 10?**

Notes

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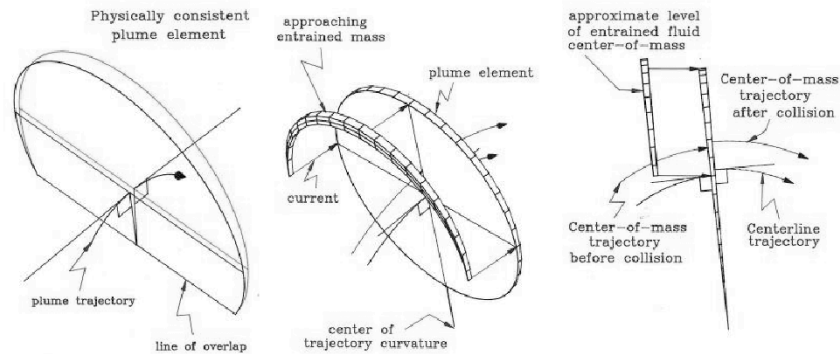
Understanding the significance of the steady state assumption ultimately lead to a completely new conception of the plume element. The right-cylinder tuna can was replaced by a section from a bent cone. The trick became to accurately derive the projected area of the plume element’s surface as a function of r , h , and θ , the trajectory inclination angle to the horizontal axis.

First assuming that the plume element height (h) was constant (the “tuna can,” right cylinder conception of the Lagrangian plume element) Winiarski and Frick formulated about 20 different entrainment functions, some leading to fabulous, but wrong, solutions, like blowing up.

After suspecting that perhaps h could not be assumed constant, W&F rather quickly formulated the current expression for forced entrainment, probably less than 5. First, an examination of Fan’s dilution and radii data confirmed that they were not directly proportional or linearly related. Something like the car analogy, followed by the rigorous integration found in the DOS Plumes manual, was then used to develop the “free” equation for h .

UM3 equations are based on the “top hat” assumption, that plume properties are average values when it comes to expressing the equations of motion. This is an idealization, obviously plume centerline properties are different from edge properties. In omitting a pressure force on the plume, they reasoned that plume properties “feathered” into ambient properties at the plume’s edge, hence no pressure force as would be experienced by a solid object.

Dream model element & entrainment



- Wedge shape and overlap (left)
- The concept of all approaching ambient fluid being captured by the plume element (middle and right)

Notes

07

44

Dream model consider mass distribution about the center of mass (not the center of the cross section). Overlap is dealt with explicitly.

Schematic diagrams illustrating details of plume merging theory; the plume element as a wedge-shaped, overlapped entity; mass about to collide with the plume to become entrained mass—part of the plume.

Model convergence scheme discontinuity

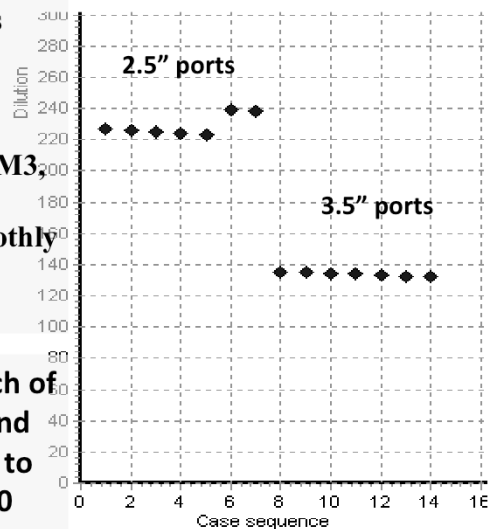
Differential equations (DE) express changes with time or distance that cannot be solved exactly (analytically).

Solving stiff equations means, in UM3, a new $\Delta t = t_2 - t_1$ each step

UM3: Δt changes gradually & smoothly

DKH: Δs changes relatively larger

Figure: Two diffuser sections. Each of the 6 dilution estimates correspond to port spacing varying from 3.66 to 3.565m, very little. Between 3.570 and 3.565m the predicted DKH dilution increases over 8%.



Which side of the discontinuity has the more accurate solution?

Notes

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Differential equations (DE) express changes with time or distance

Usually the changes are smooth and continuous

The plume DE can not be solved analytically

The DE must be solved numerically: a finite difference approach

For the Lagrangian model the infinitesimal integrating factor like dt is replaced by $\Delta t: t_2 - t_1$

For the Eulerian integral flux the infinitesimal integrating factor ds is replaced by $\Delta s: s_2 - s_1$

The numeric integration is stepwise

If Δt or Δs are too large the solution diverges from the true solution

because the Δt or Δs too crude to capture rapid changes

If Δt or Δs are too small the solution diverges from truncation errors

The plume equations are sometimes called stiff:

at first Δt or Δs must be tiny but if constant truncation errors build up

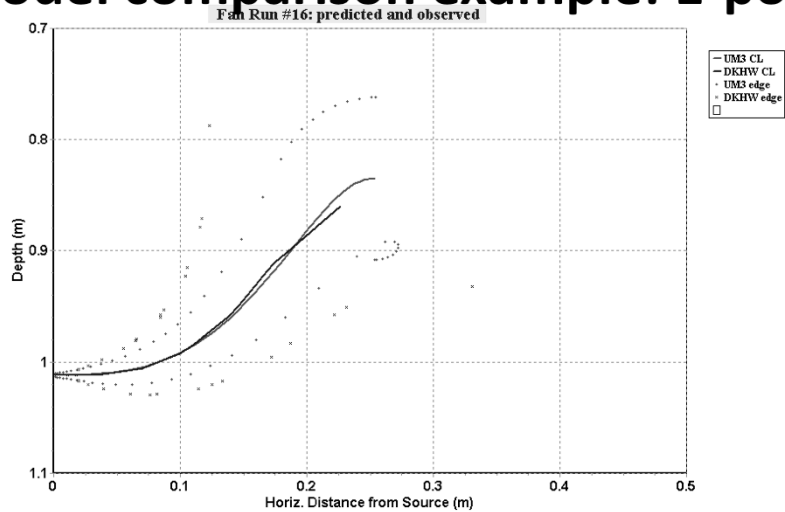
Convergence schemes are needed, for example, Δt must increase as the plume solution develops

Good increase schemes for Δt or Δs yield solutions that converge

Crude schemes cause divergence or quantum jumps, i.e., a tiny change in current angle will cause a not insignificant change in dilution prediction simply because the integrating factor adjustment was too coarse.

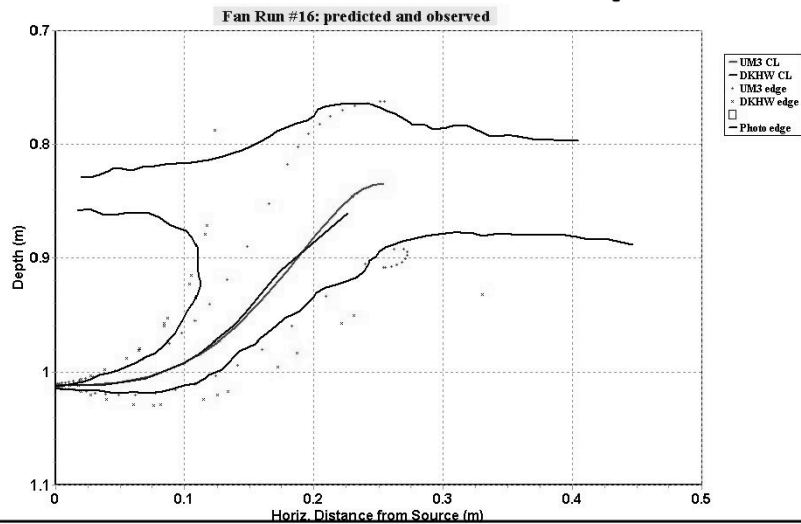
UM3 is very continuous

Model comparison example: 1-port



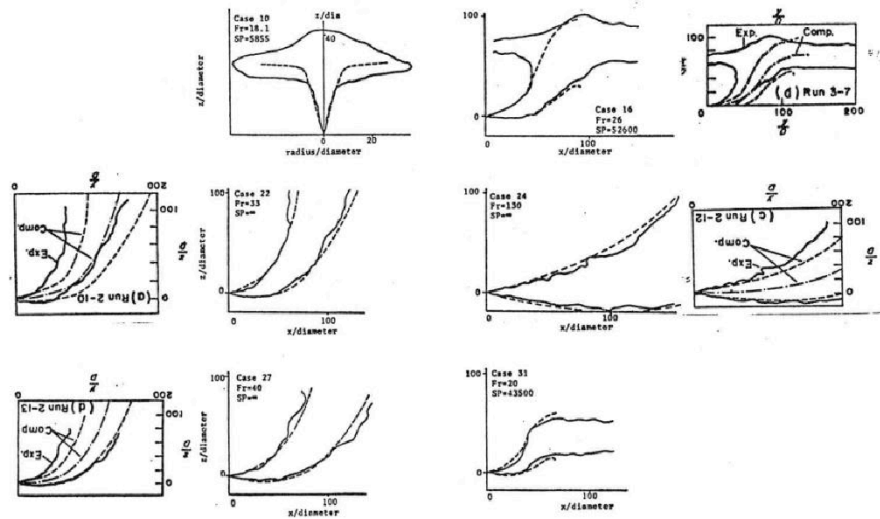
Fan Run 16 input; DKHW (blue) and UM3 (red) simulations.
Stagnant, density stratified environment.

VP verification example



Same input as previous slide. VP allows input from text files, a capability used to show the experimental plume trace.

Example UM3 verification

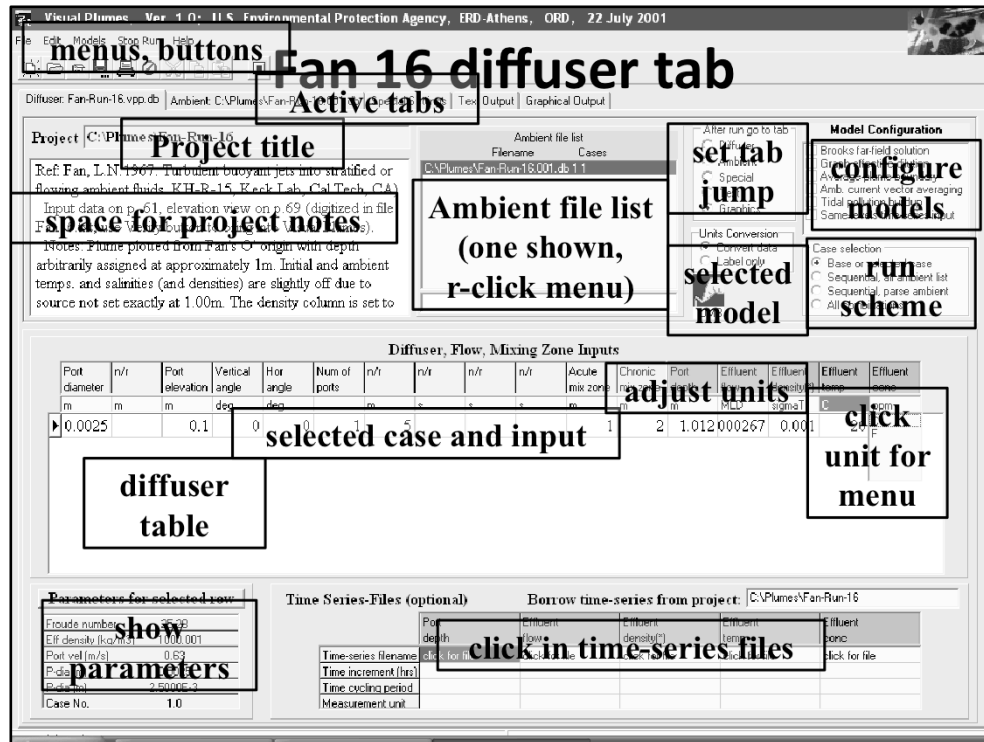


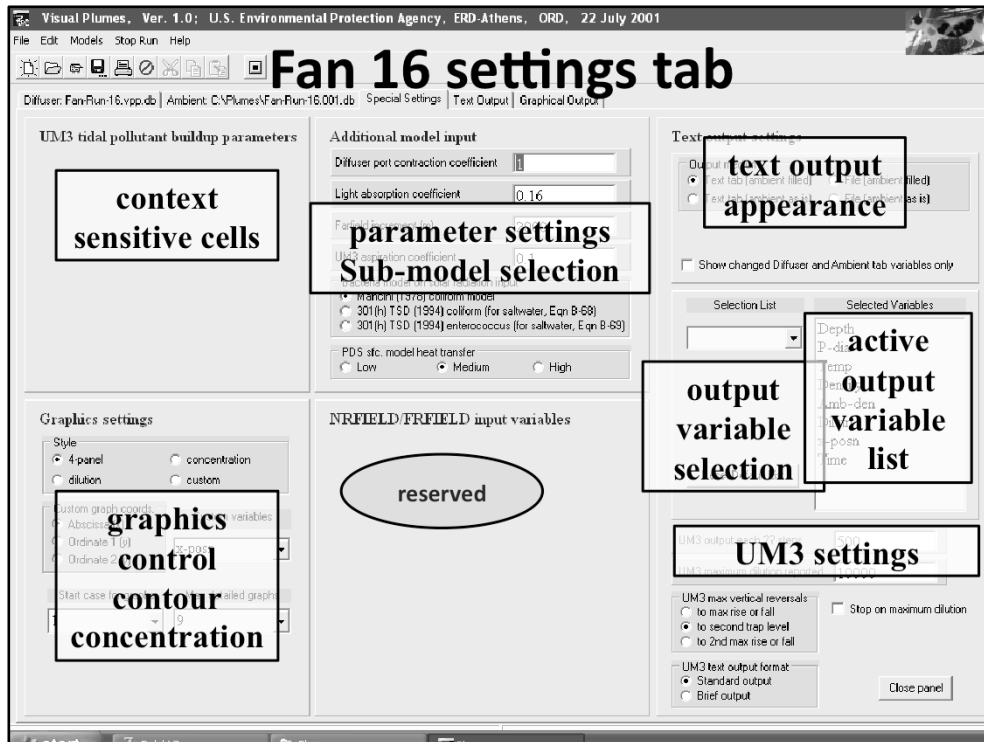
Six center panels, UMERGE (UM3 predecessor) model predictions. Schatzmann's multi-parameter model predictions in margins. Data from Fan, 1967.

Preface to the live demonstration



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Visual Plumes, Ver. 1.0; U.S. Environmental Protection Agency, ERD-Athens, ORD, 22 July 2001

File Edit Models Stop Run Help

Fan 16 text output tab, UM3

Diffuser: Fan-Run-16.vpp.db Ambient: C:\Plumes\Fan-Run-16.001.pl Special Settings Text Output Graphical Output

data post process options

model ID, case #, project ID

ambient table

Depth	Amb-cur	Amb-dir	Amb-den	Amb-c	Decay	Far-sp	Far-dir	Dispersn	Density
m	m/s	deg	psu	C	kg/kg	m/s	deg	m0.67/s2	sigma-T
0.0	0.0	0.0	25.13	20.0	0.0	-	-	0.0003	17.3
1.0	0.0	0.0	35.55	20.0	0.0	-	-	0.0003	25.2
2.0	0.0	0.0	45.86	20.0	0.0	-	-	0.0003	33.1

Diffuser table

data	P-elev	V-angle	H-angle	Route	AcuteWZ	ChannWZ	P-depth	Ttl-fls	Eff-den	Temp	Footnt
(m)	(m)	(deg)	(deg)		(m)	(m)	(m)	(m)	(sigmaT)	(C)	(ppm)
2.50E-3	0.1	0.0	0.0		0.5	0.5	0.24	1.00E-3	20.0	200.0	

Simulation

Step

Step	Depth	Trap Density	Amb-den	Dilutn	x-posn	Time	Notes
	(m)	(C) (sigmaT)	(sigmaT)	()	(m)	(s)	
0	1.000E-3	25.2943	1.0	0.0	0.0	0.0	max dilution reached
208	24.4092	24.3743	44.28	0.192	5.962	5.962	trap level
225	24.3701	24.0186	55.34	0.225	8.673	8.673	begin over
303	24.3528	23.8228	57.79	0.254	11.35	11.35	local
392	24.3305	24.0638	64.58	0.289	14.69	14.69	end
408	24.3114	24.3638	0.318	17.83	17.83	17.83	trap level

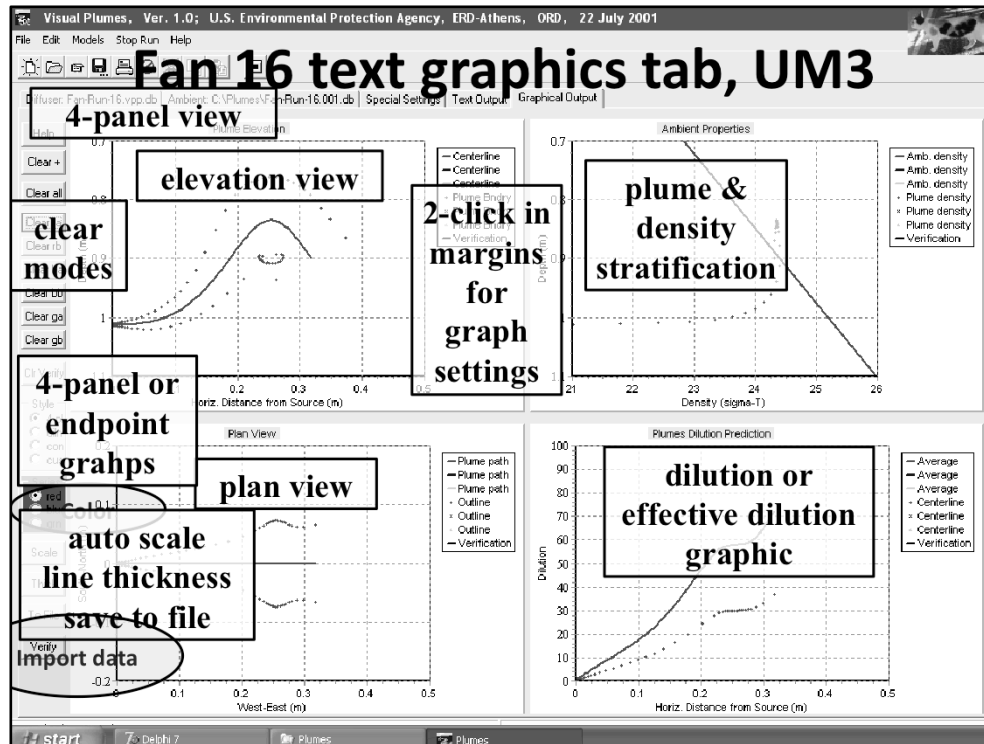
initial dilution simulation

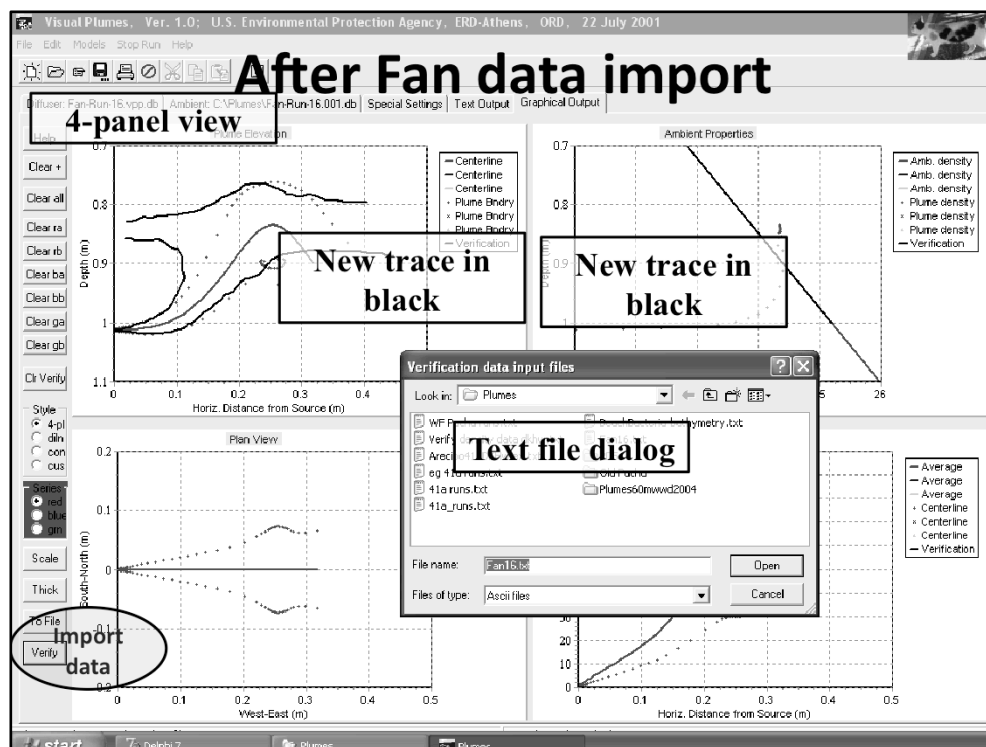
endpoint notes

Dilution factor

far-field simulation if Brooks far-field algorithm linkage is set

10:52:29 AM. amb fills: 2





data (notes)

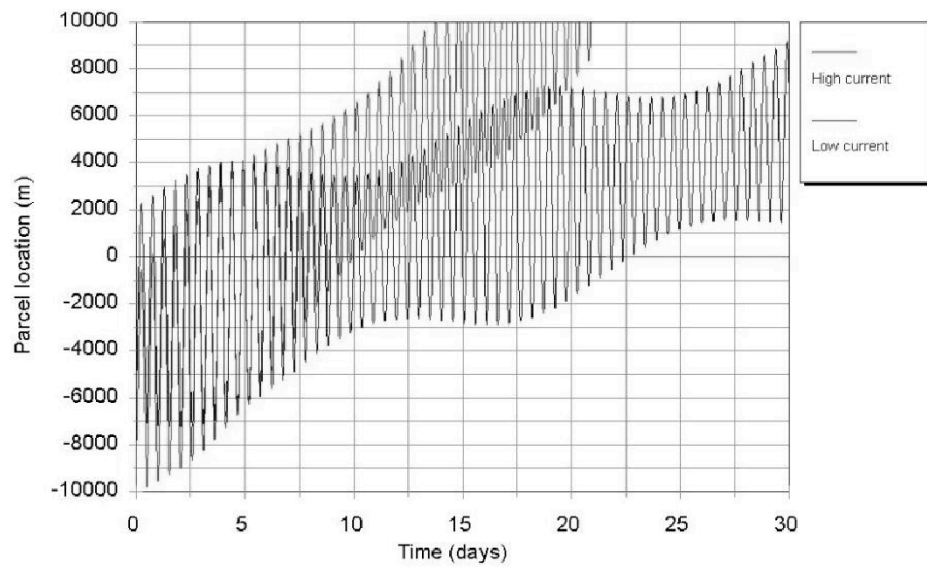
0.0170 0.8577
0.0212 0.8574
0.0278 0.8569
0.0358 0.8608
0.0459 0.8615
0.0530 0.8605
0.0630 0.8591
0.0726 0.8601
0.0808 0.8641
0.0884 0.8705
0.0953 0.8736
0.1012 0.8759
0.1061 0.8820
0.1100 0.8908
0.1105 0.8977
0.1100 0.9073
0.1101 0.9118
0.1123 0.9216
0.1124 0.9236
0.1100 0.9304
0.1073 0.9380
0.1026 0.9464
0.0997 0.9524
0.0962 0.9597
0.0924 0.9673
0.0839 0.9769
0.0777 0.9828
0.0693 0.9870
0.0624 0.9920
0.0541 0.9959
0.0485 0.9988
0.0411 1.0011
0.0343 1.0028
0.0273 1.0065
0.0212 1.0084
0.0168 1.0095
0.0099 1.0114
0.0042 1.0126
-0.0001 1.0124
density profile
17.3 0.0
25.2 1.0

Multi-run example Dominguez Channel

- Project map
- Channel

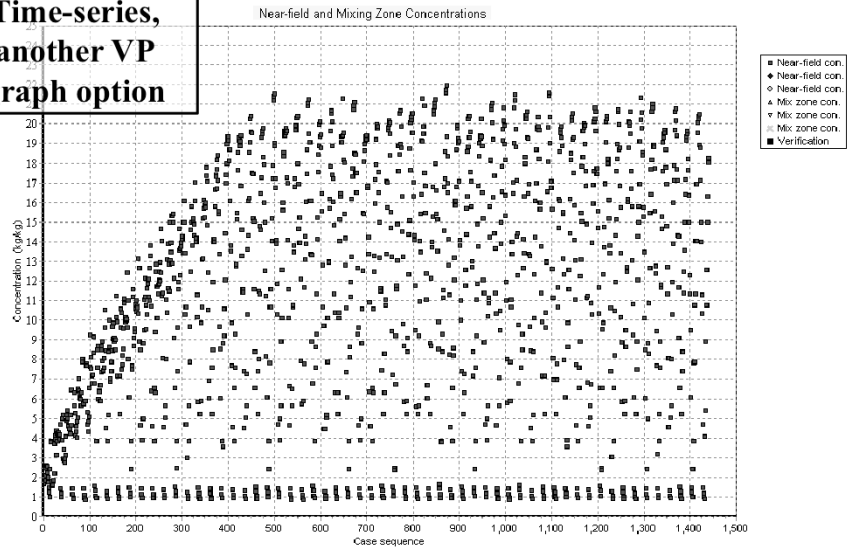


Tidal Channel Excursion



Time-Series Approach output

Time-series,
another VP
graph option



Maximum Impact

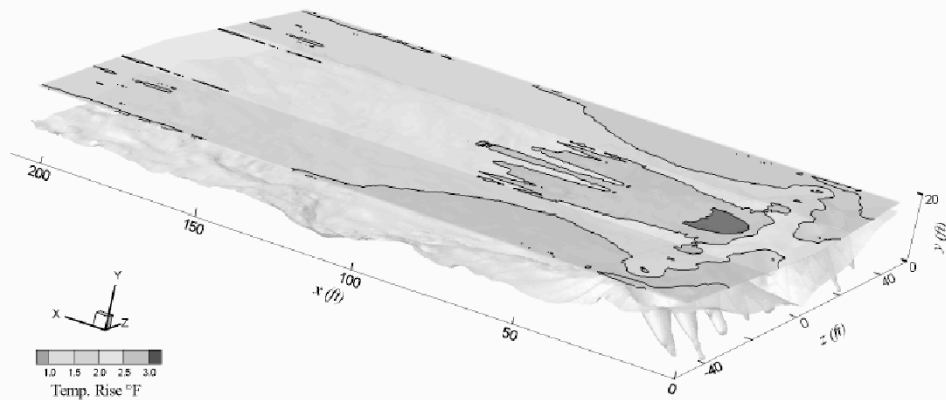


Figure 5. Perspective view of surface temperature rise.

- Surface temperature elevation hot spot

Summary

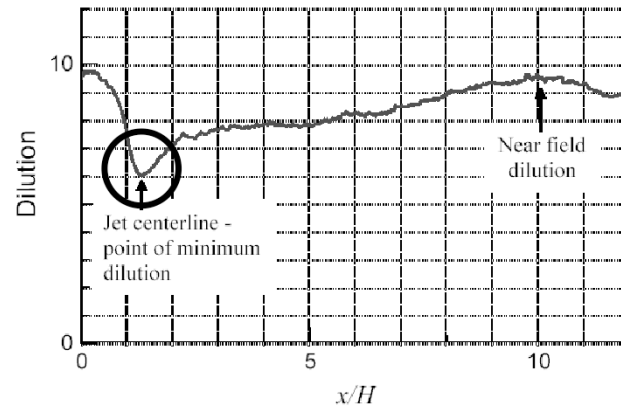
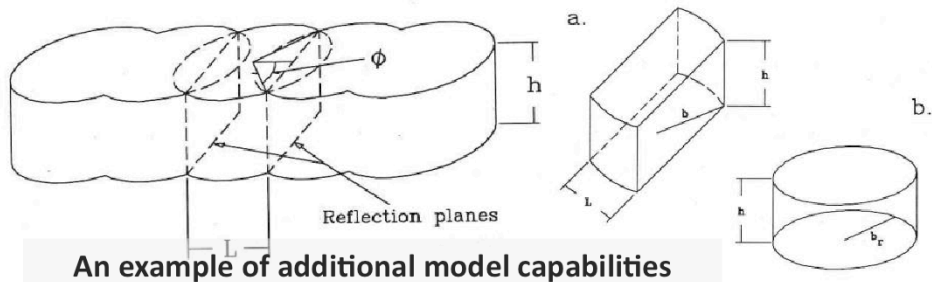


Figure 6. Variation of surface dilution with distance from the diffuser on the diffuser centerline.

- Verification? Verifying the verifier.

Simulating merging with UM3

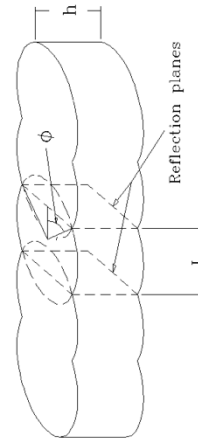


- When neighboring plumes merge, the mass is shifted in a direction perpendicular to the axis of the wastefield
- This is known as the reflection technique
- UM's algorithm is patterned after DKHw (UDKHDEN)
- In a and b, mass is conserved by this technique

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UM3 Very Shallow Water capability

- If the merging diagram is rotated 90 degrees then it is a representation for shallow water, where the bottom and surface are represented by the two planes of reflection.
- The true depth becomes associated with spacing (L in the diagram), thus spacing will represent depth.
- The width of the water body (river, channel) becomes associated with the depth.



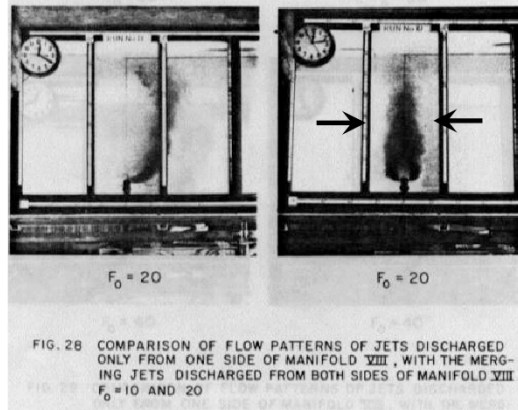
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Model limitations

Liseth experiments in zero current

Zero current worst case: viable?

Single plume
trajectory:
ambient
current = zero



Same plume in the
presence of its
opposite twin:
“ambient” current
(red arrows) is no
longer zero

**When plumes aspirate they generate inflowing current nearby.
Self-induced current is not addressed by VP models.**

Notes

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Work done by Liseth (reference not immediately available) shows plumes generate current around themselves. Here identical single and double plumes of equal densimetric Froude are shown in two sets of experiments. It is striking how in pairs the plumes “attract” each other.

References and acknowledgements

1) To be completed...

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Conclusions and Recommendations



- 1) **Visual Plumes, model manager, native and callable (exe) models**
- 2) **Ease of use: sparse input, units conversion, time-series files...**
- 3) **Public domain, inter-model comparison**
- 4) **Plume morphology, steady state and the “free” equation (jse)**
- 5) **Strong basic physics, finite difference models, Lagrangian (UM3, native) and Eulerian (DKH, exe)**
- 6) **Dimensional model empirical NRFIELD, multi-port T-riser diffusers; ongoing research on dense plumes**
- 7) **Linkage to Brooks far-field equations**
- 8) **DOS Plumes: legacy UM and RSB, similarity parameters, Very Shallow Water (VSW) technique and Cormix classes**
- 9) **Extensive guidance, DOS and Visual Plumes**
- 10) **Mixing zone course documentation (Frick et al. 2005) illustrates the use of the PDS as well as the other models**

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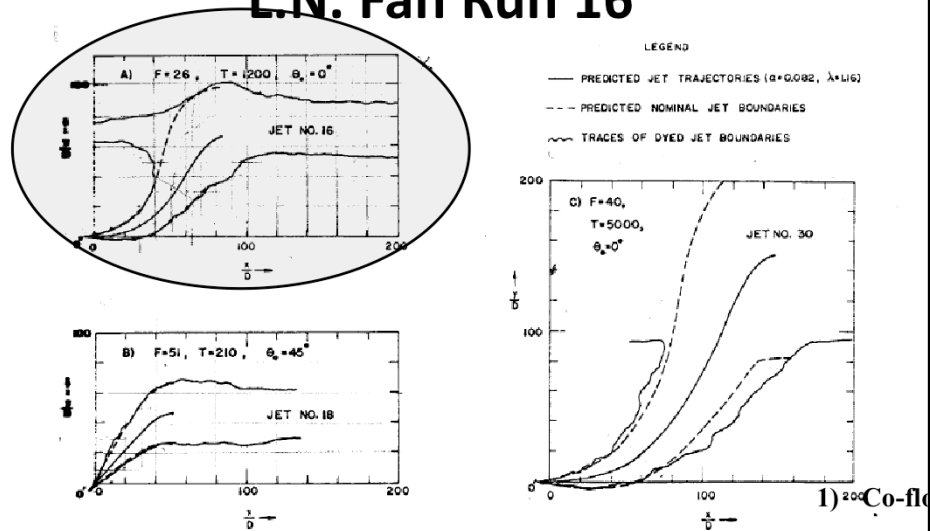
Conclusions and Recommendations continued

- 1) Visual Plumes has capabilities and flaws**
- 2) Can operating system problems be solved?**
- 3) Resources**
- 4) Can progress be propagated?**
- 5) Diversity is honesty**
- 6) Answers meaningful in conflicting contexts**
- 7) Progress more certain**
- 8) Replacing VP? Inevitable**
- 9) User facilities, physics, multi-model, partnership....**
A concept worth improving and refining

Thank you

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L.N. Fan Run 16



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Table 1. Summary of Experiments on Round Jets in Stagnant Environments

Jet Number	Initial Jet Values					Ambient Reference Density (ρ_a)	Density Gradient $\frac{1}{\rho_a} \frac{d\rho_a}{dy}$	Jet Reynolds Number $R = \frac{U_0 D}{\nu}$	Jet Froude Number F Eq. (51)	Stratification Parameter T Eq. (52)	Reference for Detailed Results
	Angle θ_0 deg.	Diameter D cm	Discharge Q_0 cc/sec	Velocity U_0 cm/sec	Density ρ_0 g/ml						
1	45	0.69	7.9	21.4	1.0087	1.0004	16.325	1,500	9.1	48	23, 24a
2	45	0.69	23	62	1.0087	1.0004	16.325	4,300	26	48	24b
3	0	0.69	17	46	1.0087	1.0005	25	3,200	20	48	--
4	90	0.69	29	79	1.0087	1.00125	25	5,400	35	44	--
5	0	0.22	4.3	110	1.0230	1.0048	50	2,500	55	160	--
6	26.7	0.22	4.3	109	1.0230	1.0036	50	2,400	53	170	--
7	90	0.22	8.2	105	1.0230	1.0046	50	2,300	53	160	--
8	54.5	0.22	8.7	111	1.0230	1.0038	50	2,500	54	170	--
9	-25	0.22	8.9	114	1.0230	1.0046	50	2,500	57	160	--
10	90	0.46	8.4	50	1.0240	1.0070	36.5	2,300	18	100	22
11	43.6	0.46	10.2	61	1.0240	1.0059	36.5	2,800	21	107	25a
12	2.8	0.46	6.4	38	1.0240	1.0052	36.5	1,800	13	110	25b
13	-28.2	0.46	6.4	38	1.0240	1.0082	36.5	1,800	14	93	--
14	-28.2	0.46	10.2	61	1.0240	1.0082	36.5	2,800	23	93	--
15	39.1	0.46	9.7	58	1.0240	1.0062	36.5	2,700	20	106	25c
16	0	0.25	3.1	64	1.0010	1.0010	17.5	1,600	26	1,200	26a
17	0	0.25	4.8	99	1.0175	1.0021	29.5	1,900	51	210	21, 26b
18	45	0.25	4.8	99	1.0175	1.0021	29.5	1,900	51	210	--
19	0	0.25	--	--	1.0030	1.0030	0	--	infinite (2)	--	--
20	0	0.25	--	--	1.0015	1.0015	0	--	infinite (2)	--	31
21	0	0.25	--	--	1.0015	1.0015	0	--	infinite (2)	--	31
22	0	0.25	2.5	51	1.0101	1.0000	0	1,300	33	infinite (3)	29a
23	0	0.25	5.0	101	1.0101	1.0000	0	2,600	66	infinite (3)	30a
24	0	0.25	10.5	205	1.0101	1.0000	0	5,200	130	infinite (3)	30b
25	0	0.25	2.6	53	1.118	1.000	0	1,300	10	infinite (3)	29b
26	0	0.25	3.5	73	1.118	1.000	0	1,800	13.6	infinite (3)	29c
27	0	0.25	10.6	214	1.118	1.000	0	5,300	40	infinite (3)	30c
28	0	0.25	5.3	53	1.118	1.001	9.5	1,300	10	5,000	--
29	0	0.25	3.5	73	1.118	1.001	9.5	1,800	13.6	5,000	--
30	0	0.25	10.6	214	1.118	1.001	9.5	5,300	40	5,000	26c
31	0	0.25	1.8	36	1.0134	1.0013	9.5	900	20	510	27a
32	0	0.25	3.5	72	1.0134	1.0013	9.5	1,800	40	510	27b
33	0	0.25	5.4	104	1.0134	1.0013	9.5	2,700	60	510	27c

Note:

1) ρ_a is taken to be the ambient density at the level of the nozzle

2) F = infinity refers to a simple jet

3) T = infinity refers to a buoyant jet in a uniform environment

Fan Run 16 data

Diffuser: FanRun16.vpp.db
Ambient: C:\Plumes\FanRun16.001.db
Special Settings
Text Output
Graphical Output

Project C:\Plumes\Fan-Run-16

Ref: Fan, L.N.1967. Turbulent buoyant jets into stratified or flowing ambient fluids. KH-R-15, Keck Lab, Cal Tech, CA)

Input data on p. 61, elevation view on p.69 (digitized in file Fan16.txt; use Verify button to bring into Visual Plumes).

Notes: Plume plotted from Fan's O' origin with depth arbitrarily assigned at approximately 1m. Initial and ambient temps. and salinities (and densities) are slightly off due to source not set exactly at 1.00m. The density column is set to

Ambient file list

Filename	Cases
C:\Plumes\FanRun16.001.db 1.1	
C:\Plumes\FanRun16.002.db 1.1	

Model Configuration

After run go to tab:

- ☐ Diffuser
- ☐ Ambient
- ☐ Special
- ☐ Text
- ☒ Graphics

Units Conversion:

- ☒ Convert data
- ☐ Label only

UM3

Model Configuration:

- ☐ Brooks far-field solution
- ☐ Graph effective dilution
- ☐ Average plume boundary
- ☐ Amb. current vector averaging
- ☐ Tidal pollution buildup
- ☐ Same-levels time-series input

Case selection:

- ☒ Base or selected case
- ☐ Sequential, all ambient list
- ☐ Sequential, parse ambient
- ☐ All combinations

Additional model input

Diffuser port contraction coefficient:

Light absorption coefficient:

Farfield increment (m):

UM3 aspiration coefficient:

Bacteria model on solar radiation input:

- ☒ Mancini (1978) coliform model
- ☐ 30T(p) TSD (1994) coliform (for saltwater, Eqn B-68)
- ☐ 30T(p) TSD (1994) enterococcus (for saltwater, Eqn B-69)

DINO solar radiation model:

Selection List:

Selected Variables:

- ☐ Depth
- ☐ P-dia
- ☐ Temp
- ☐ Density
- ☐ Amb-den
- ☐ Dirm
- ☐ x-posn
- ☐ Time

Reset Default List

UM3 output each ?? steps:

UM3 maximum dilution reported:

UM3 max vertical reversal:

- ☐ to max rise or fall
- ☒ to second trap level
- ☐ to 2nd max rise or fall

UM3 text output format:

- ☒ Standard output
- ☐ Brief output

Close panel

Diffuser, Flow, Mixing Zone Inputs

Port diameter	n/h	Port elevation	Vertical angle	Hor angle	Num of ports	n/h	n/h	n/h	n/h	Acute mix zone	Chronic mix zone	Port depth	Effluent flow	Effluent density(°)	Effluent temp	Effluent conc
m		m	deg	deg		m	s	s	s	m	m	m	bb/d	sigmaT	C	ppm
0.0025		0.1	0	0	1	5				1	2	1.012	1.6794	0.001	20	100
													3.2			

Fan Run 16 VP input

Measurement	Current	Current	Ambient	Ambient	Background	Pollutant	n/h	n/h	Far-field
depth or height	speed	direction	salinity	temperature	concentration	decay rate(°)			dilution coeff
Depth or Height	depth	depth	depth	depth	depth	depth	depth	depth	depth
Extrapolation (sic)	constant	constant	constant	constant	constant	constant	constant	constant	constant
Extrapolation (bmi)	constant	constant	extrapolated	constant	constant	constant	constant	constant	constant
Measurement unit	m/s	deg	sigmaT	C	ppm	s-1	m/s	deg	mD.67/h2
	0	0	17.3	20	0	0			0.0003
1			25.2	20					
2									

Ambient file list
Filename
FanRun16.001.db 1.1

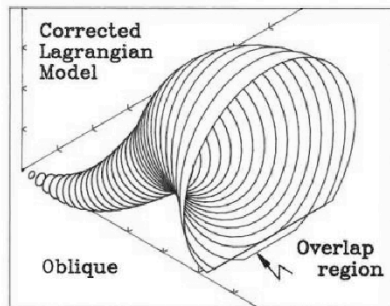
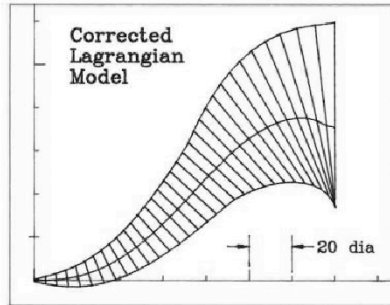
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Worst Case

- 1) Co-flow conditions are not generally worst case for multi-port diffusers
 - 1) Current direction is important
- 2) Integral models should account for variable plume spacing
- 3) Existing models sometimes can be used in a way to compensate for these deficiencies where they exist:
 - 1) As in DOS Plumes, input reduced spacing instead of port spacing
 - 2) Post-process output to determine dilution at the point of plume impact
- 4) And, not explicitly addressed here, the plume centerline should not be used to determine when plumes surface (rather the plume edge)
- 5) Also, if using weighted average dilution as a measure of overall diffuser performance, merged plumes should be considered in aggregate
- 6) VP provides a time-series capability useful for better identifying worst-case conditions

Bonus
slide

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Vector Lagrangian model: Mathematical and Physical necessities

- 1) UM3 simulates the overall “average behavior” of the plume along the plume trajectory
- 2) Wire frame depiction conforms roughly to the idea or the shape of the plume element
- 3) However, the equal spacing between cross-sections does not conform to maintaining only effluent particles in the plume element defined at the source
- 4) Typically plume effluent velocities exceed current velocities and hence the plume element tends to decrease with distance from the source
 - 1) This implies the leading edge of the element has a lesser velocity than the trailing edge
 - 2) By mass continuity, the plume element radius grows from this velocity convergence (the jelly-sandwich equation)

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Bonus
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